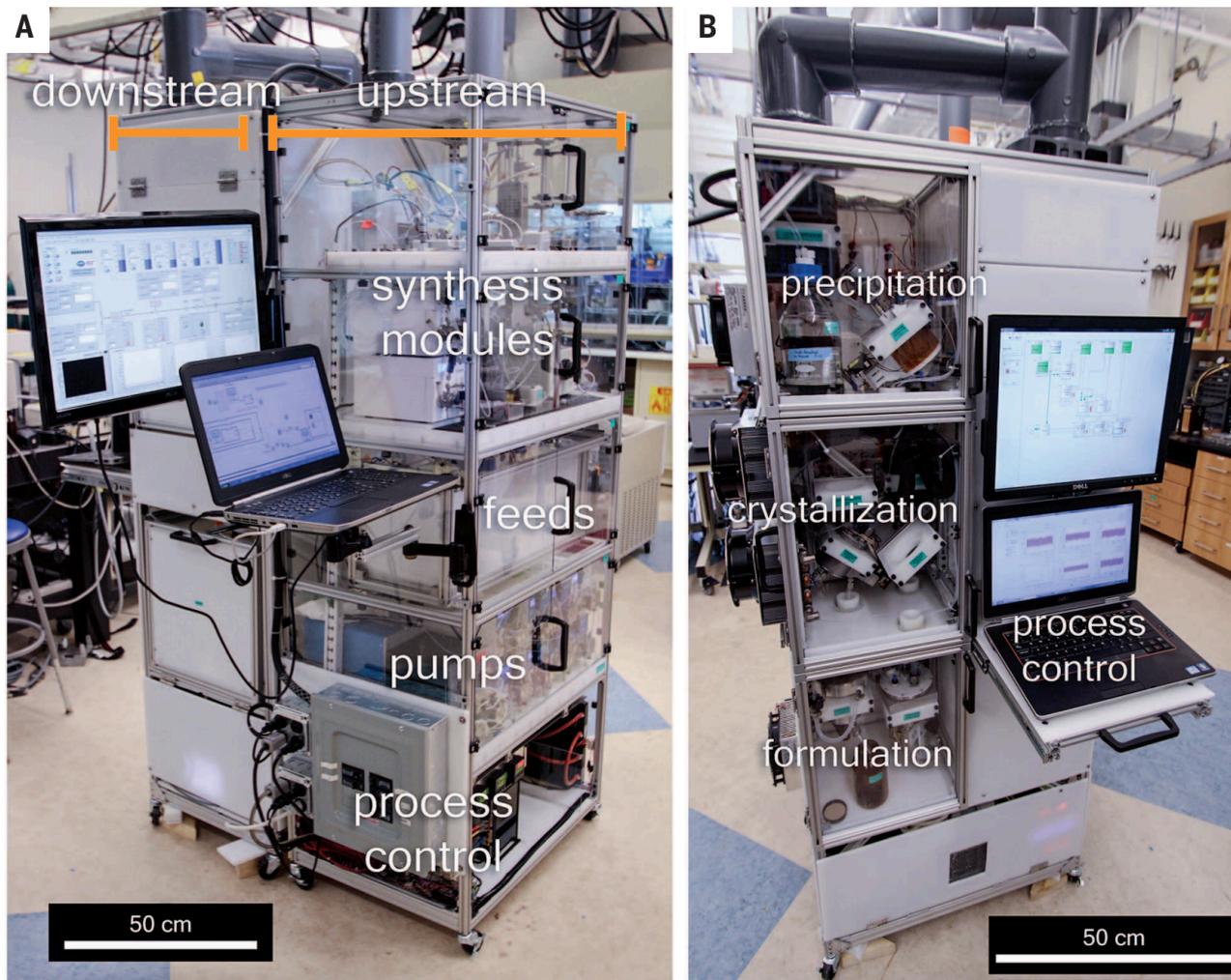


# Introduction to Flow Chemistry



Eric Alexy  
Literature Meeting  
December 14<sup>th</sup>, 2018

# *Introduction to Flow Chemistry*



Eric Alexy  
Literature Meeting  
December 14<sup>th</sup>, 2018

# *Overview*

## I. flow chemistry basics and common techniques

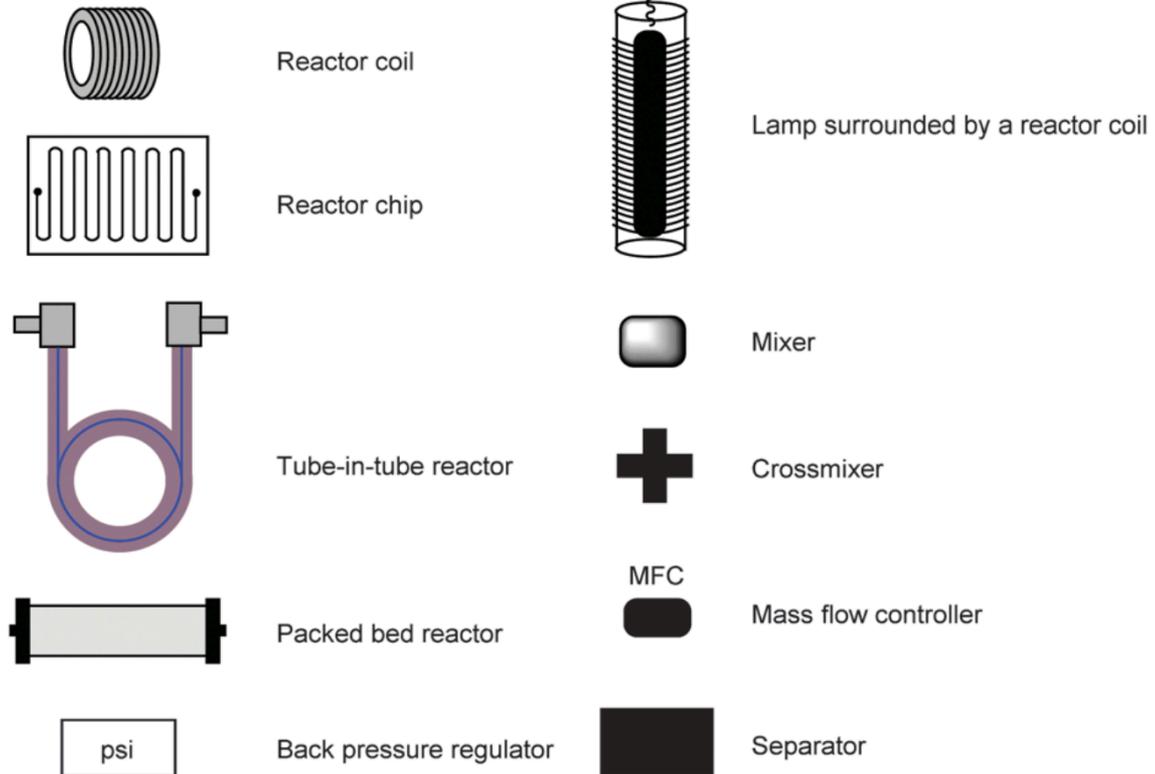
- types of reactors
- continuous extraction and other purification methods

## II. selected examples of flow synthetic methodology

## III. application of flow chemistry toward API/natural product synthesis

- one-step processes
- multi-step continuous processes

# Overview



# Overview

Reactor



T mixer



Y mixer



Quad mixer



Check valve



Union



Back-pressure regulator



Static mixer



Molecular sieve column



Packed-bed column



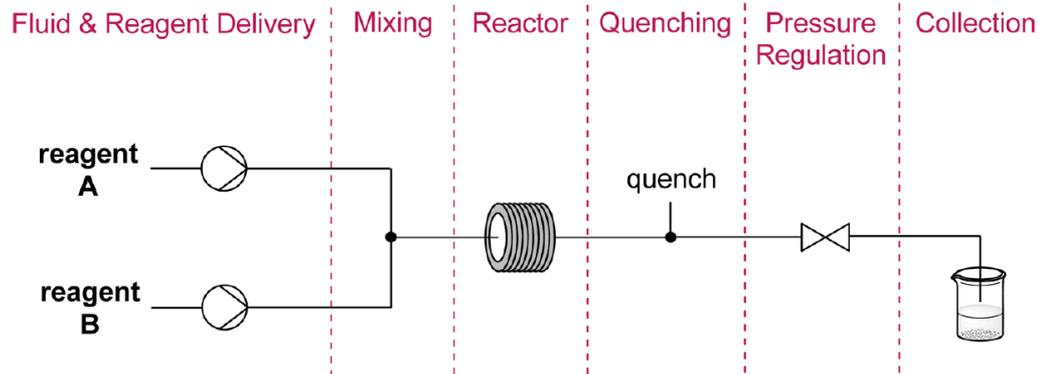
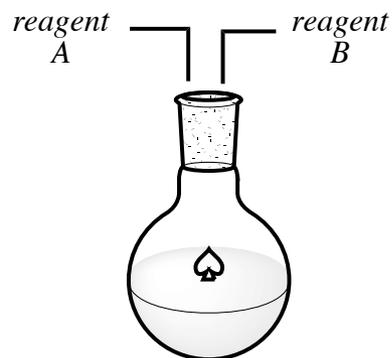
Liquid-liquid separator



Pump



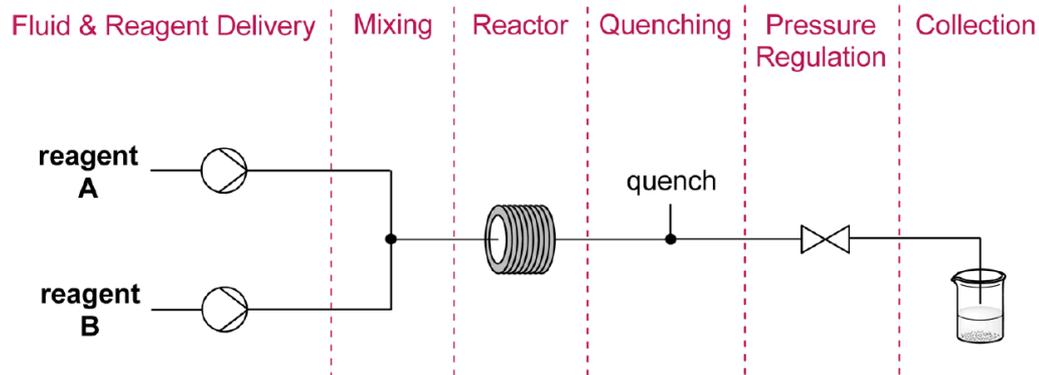
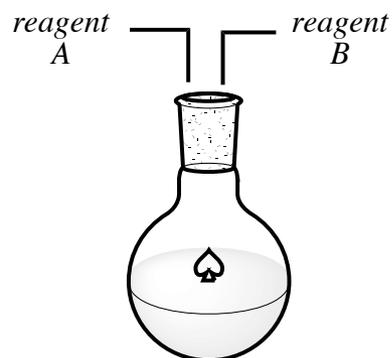
# Batch vs. Flow



key advantages of flow

- optimal heat transfer due to high surface area
- accelerated mixing/micromixing
- easy use of high pressure: heating solvents above their boiling point
- continuous setup requires minimal intervention once initiated
- increased performance of multiphasic reactions

# Batch vs. Flow

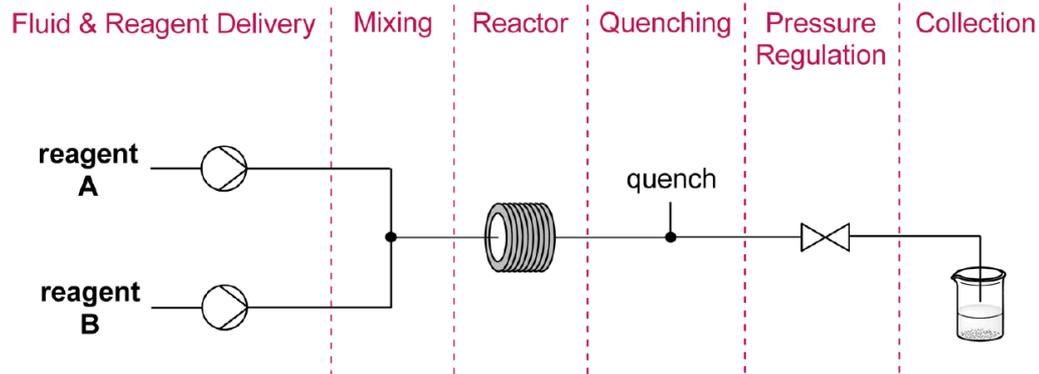
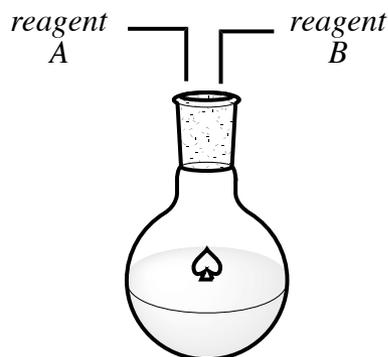


key advantages of flow

- optimal heat transfer due to high surface area
- accelerated mixing/micromixing
- easy use of high pressure: heating solvents above their boiling point
- continuous setup requires minimal intervention once initiated
- increased performance of multiphasic reactions

*both involve the same fundamental operations*

# Batch vs. Flow



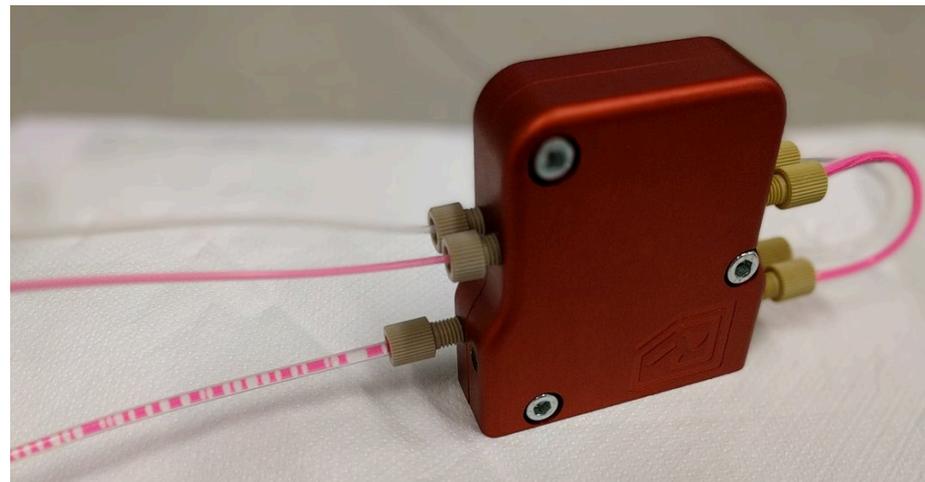
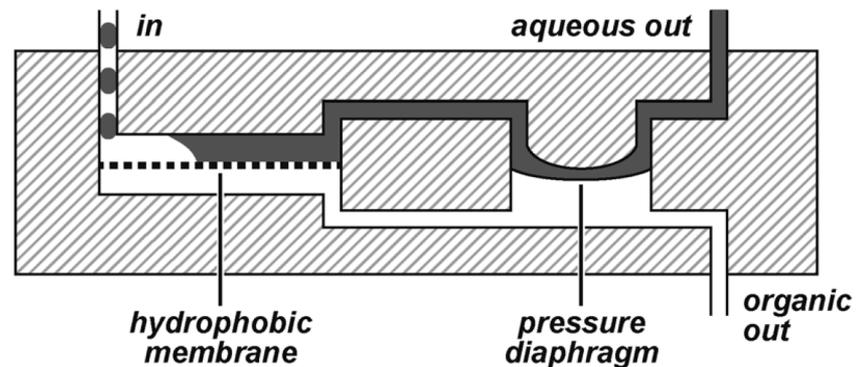
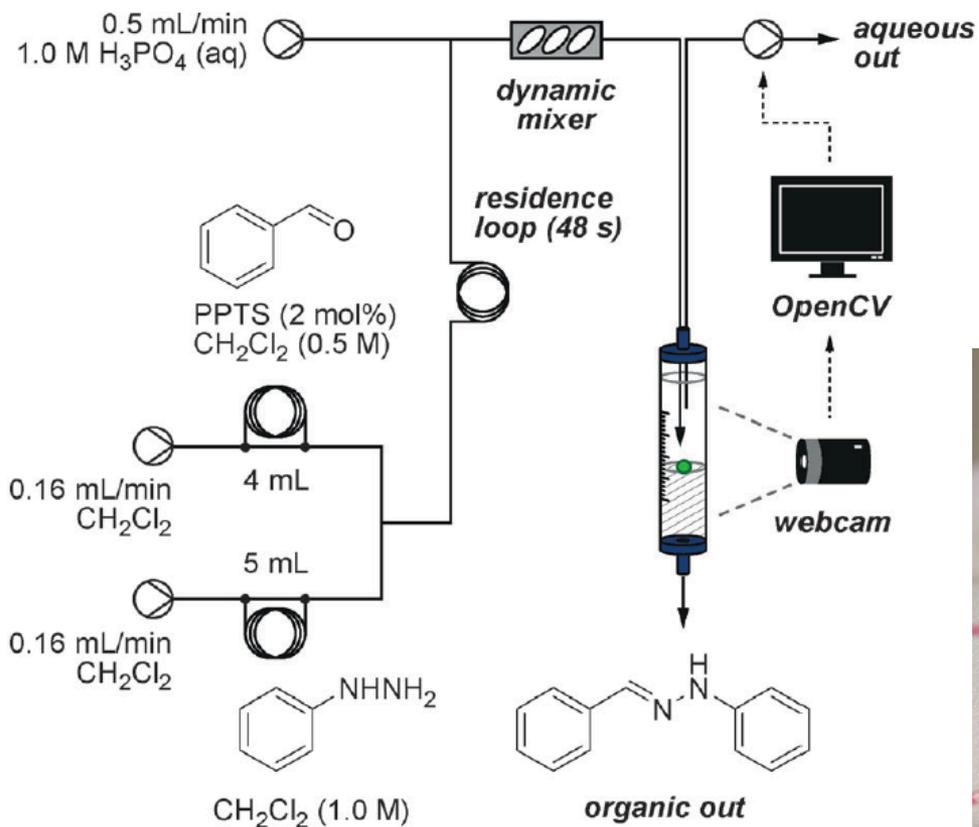
key advantages of flow

- optimal heat trans
- accelerated mixing
- easy use of high p
- continuous setup
- increased performance of multiphasic reactions

***“A machine-assisted approach gives people more time to think plan, and make discoveries.”***  
***-Steve Ley***

*both involve the same fundamental operations*

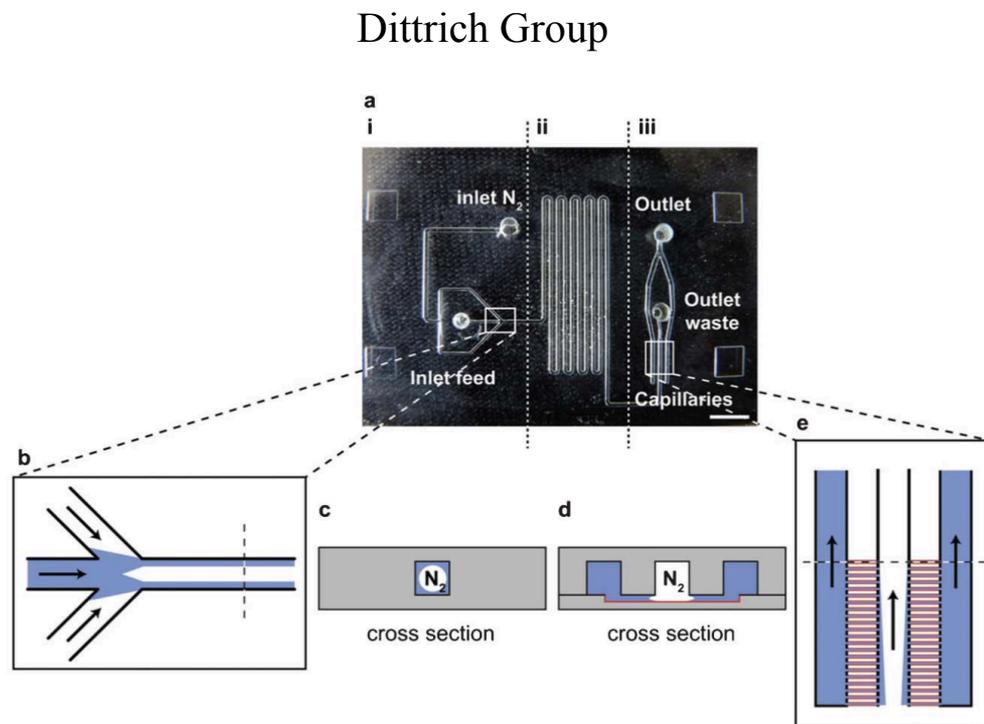
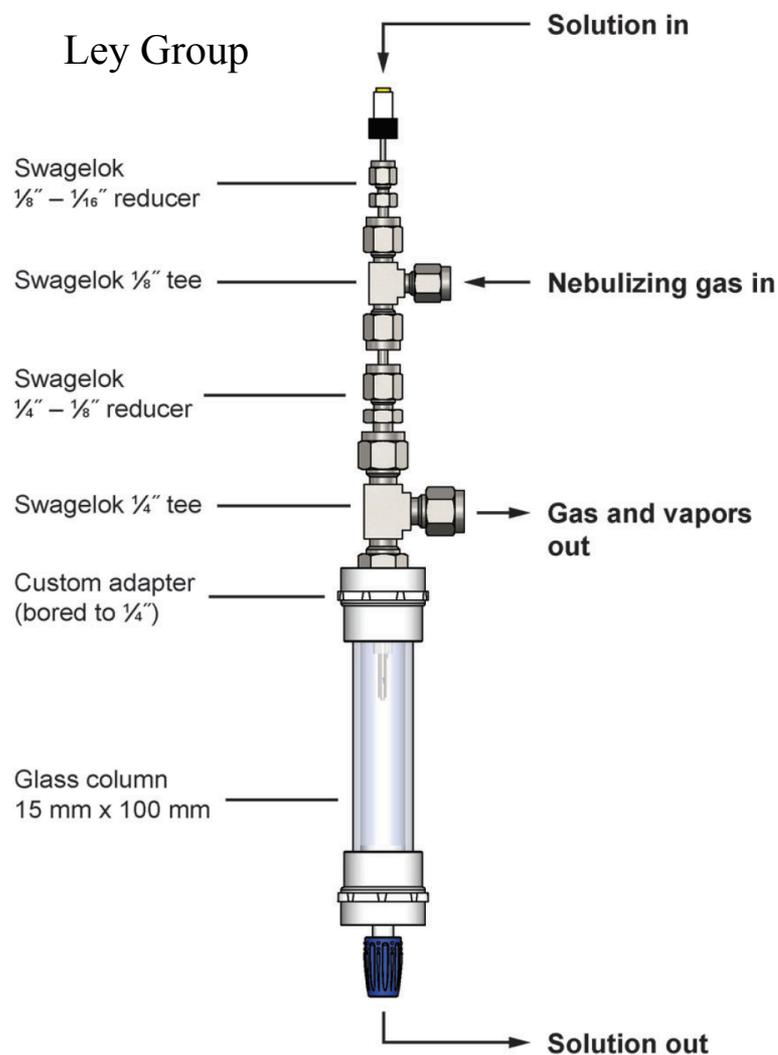
# Liquid-Liquid Extraction



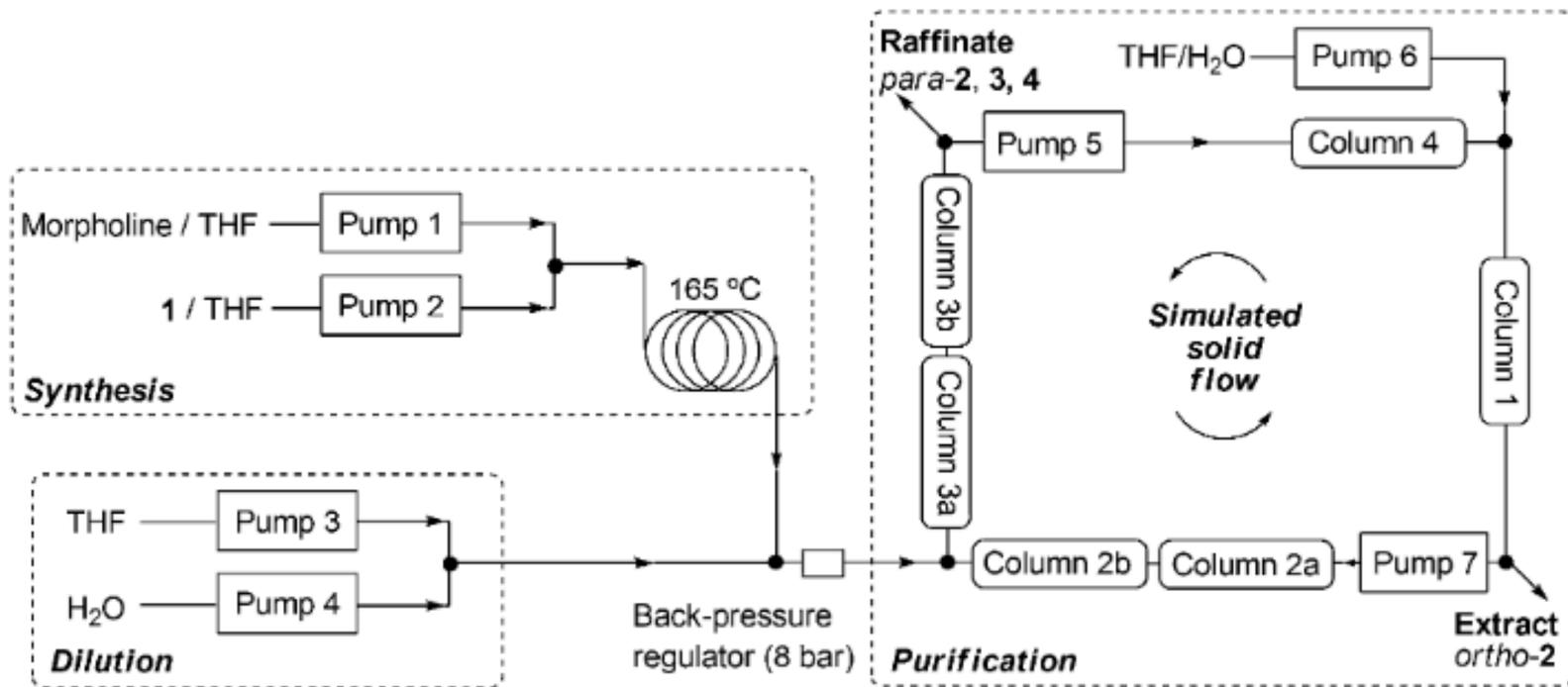
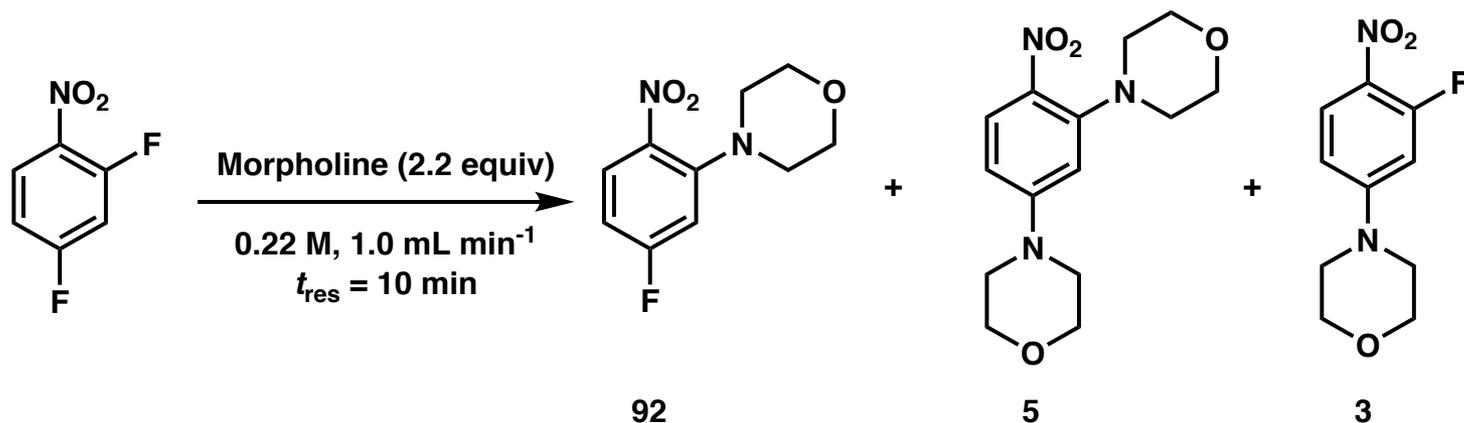
Hu, O'Brien, *Ley Org. Lett.* **2012**, *14*, 4246–4249.

Ley, Fitzpatrick, Ingham, Myers *Angew. Chem., Int. Ed.* **2015**, *54*, 3449–3464.

# In-Line Solvent Removal/Swap

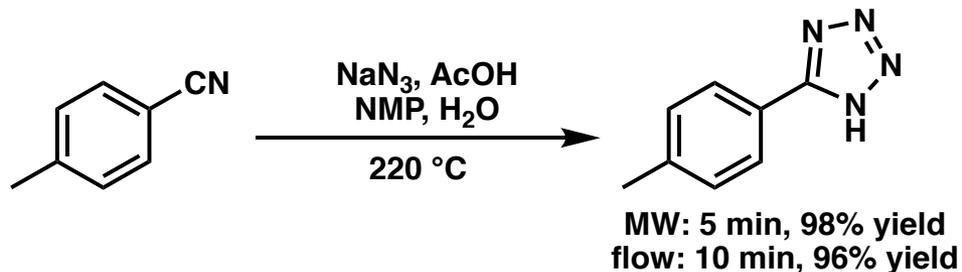


# Simulated Moving-Bed (SMB) Chromatography

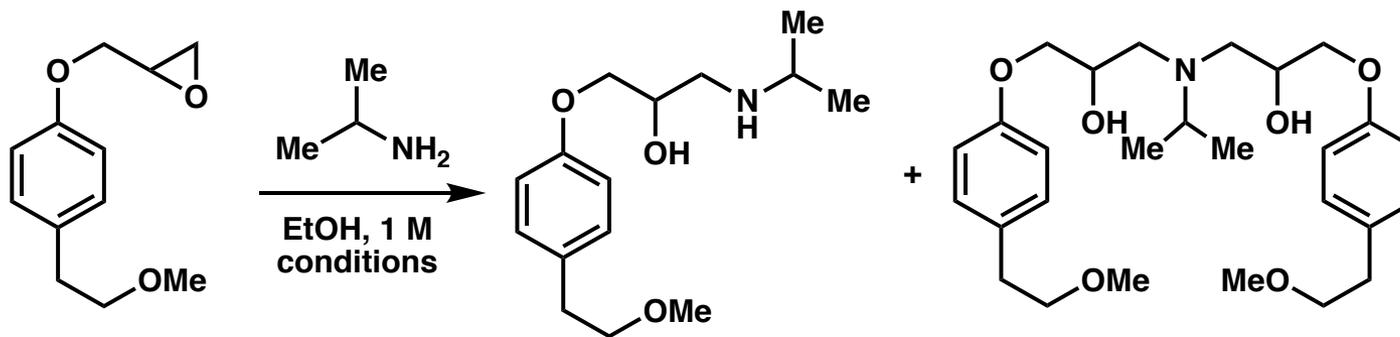


# Microwave-to-Flow Paradigm

-paradigm states that reactions optimized in MW conditions easily translate to flow

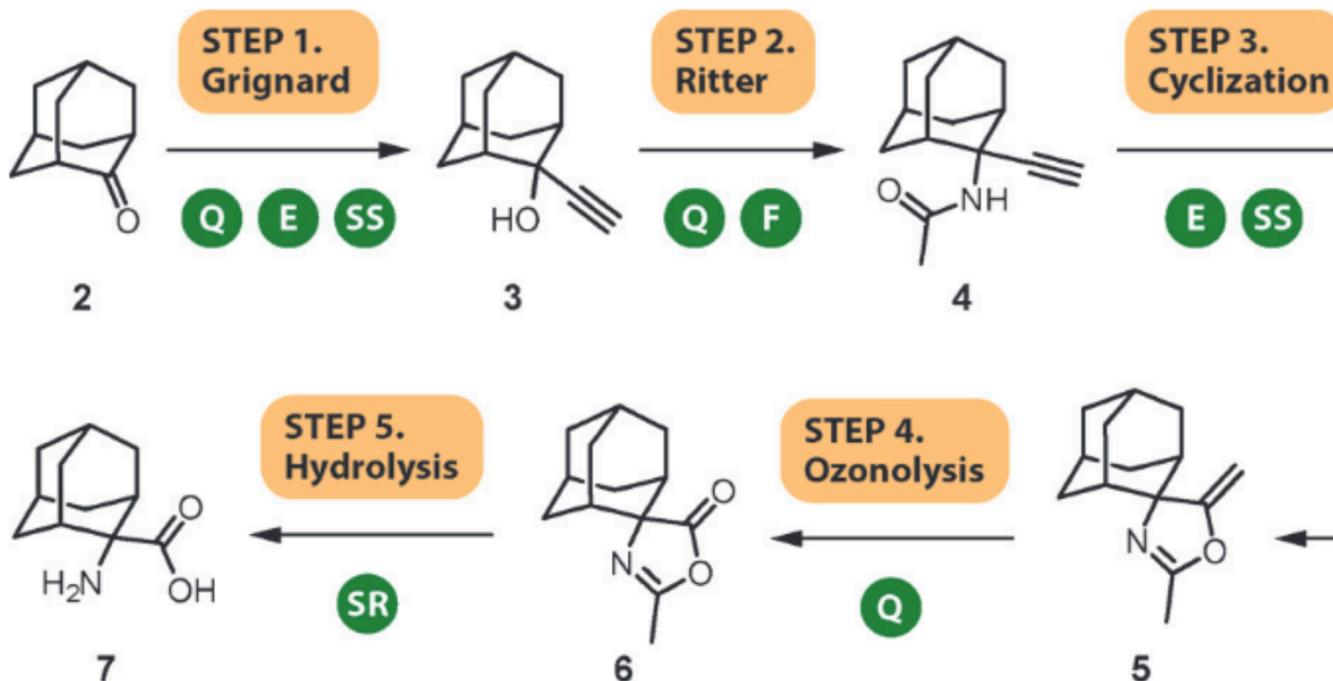


-in situ formation of toxic hydrazoic acid (HN<sub>3</sub>)



| entry | conditions (psi) | amine equiv | temp °C | time   | yield A | yield B |
|-------|------------------|-------------|---------|--------|---------|---------|
| 1     | batch MW (100)   | 1.2         | 150     | 30 min | 69      | 28      |
| 2     | flow (500)       | 4.0         | 240     | 15 s   | 91      | 6       |

# Integrated Operations

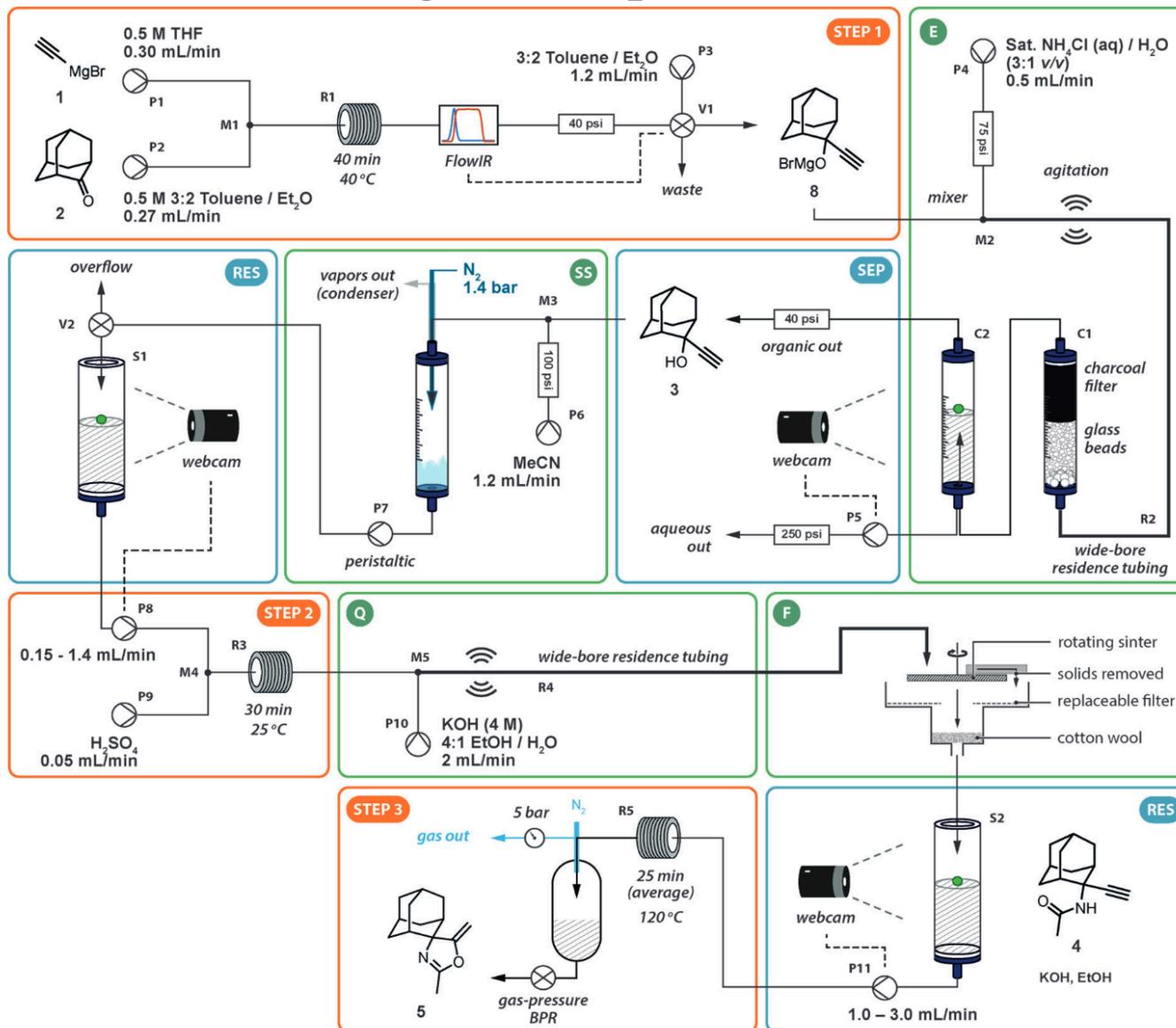


Q = quench  
E = extraction

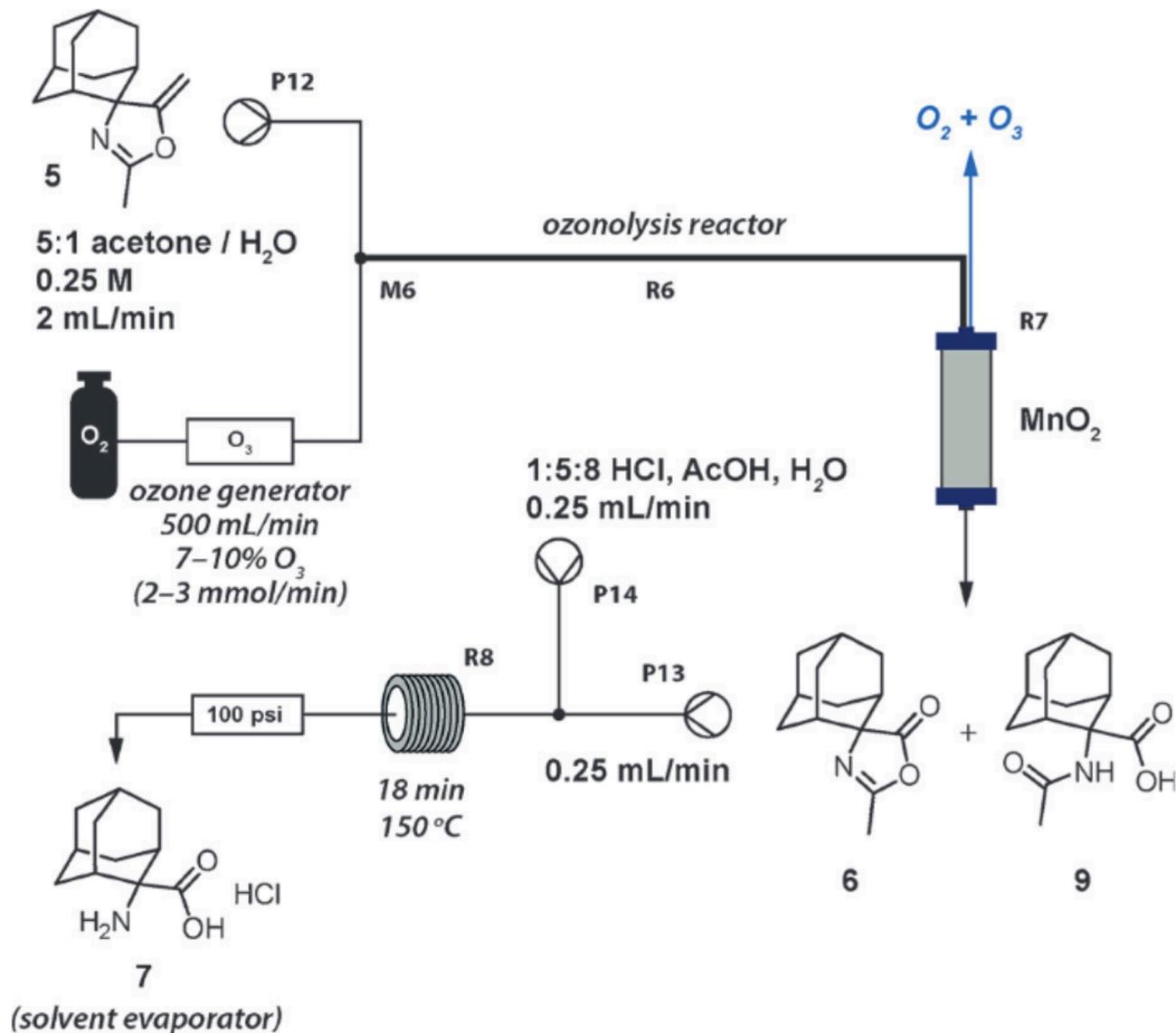
SS = solvent switch  
F = filtration

SR = solvent removal

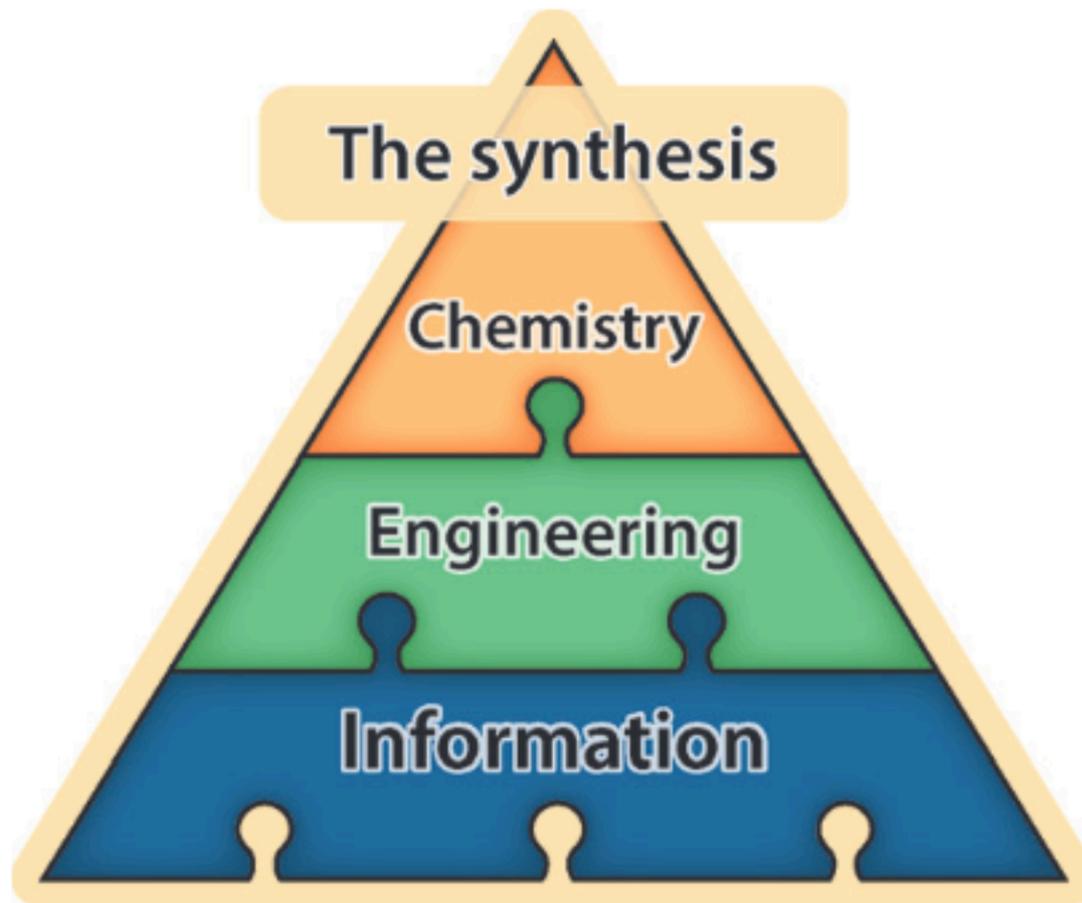
# Integrated Operations



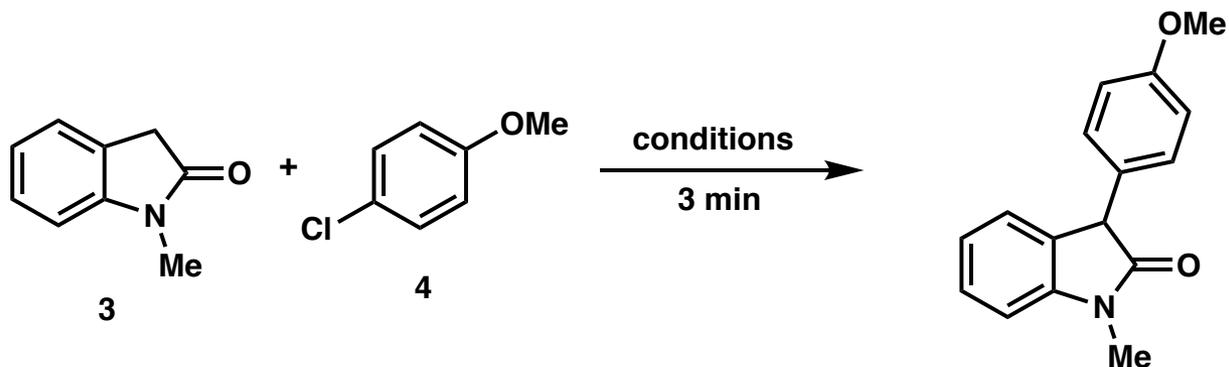
# Integrated Operations



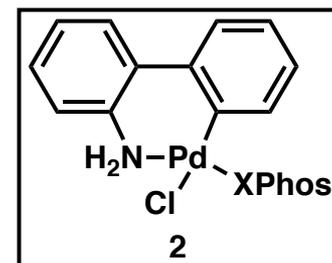
# *Integrated Operations*



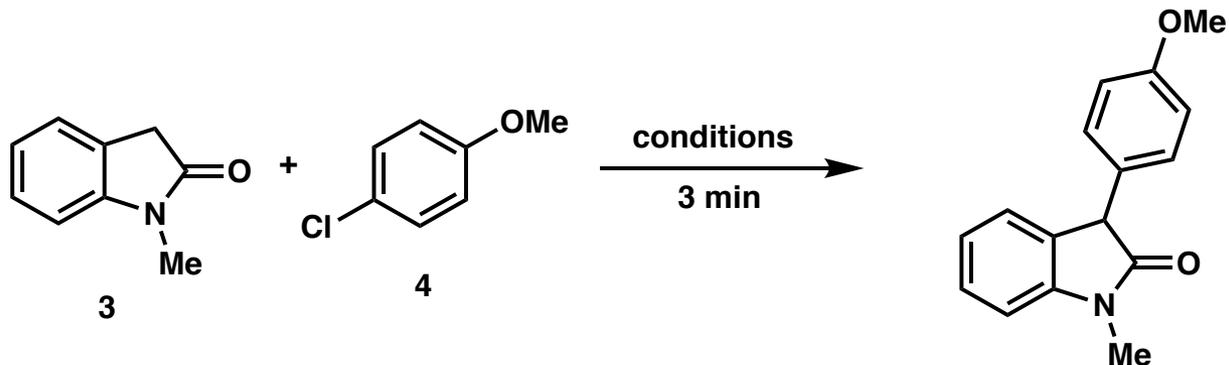
# Packed-Bed Reactor



| entry | Pd Source (1 mol %)  | Base                    | Solvent              | Yield |
|-------|----------------------|-------------------------|----------------------|-------|
| 1     | Pd(dba) <sub>2</sub> | KHMDS                   | THF/Tol              | <5    |
| 2     | Pd(dba) <sub>2</sub> | LiMHDS                  | THF/Tol              | 12    |
| 3     | 2                    | LiHMDS                  | THF/Tol              | 5     |
| 4     | 2                    | 2.0 M KOH<br>*with TBAB | Tol/H <sub>2</sub> O | 91    |

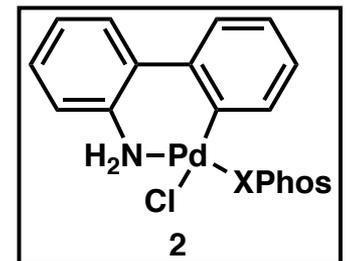


# Packed-Bed Reactor

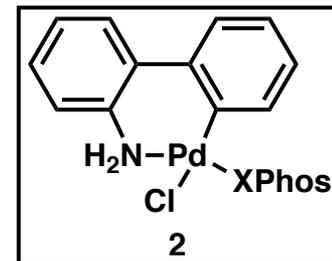
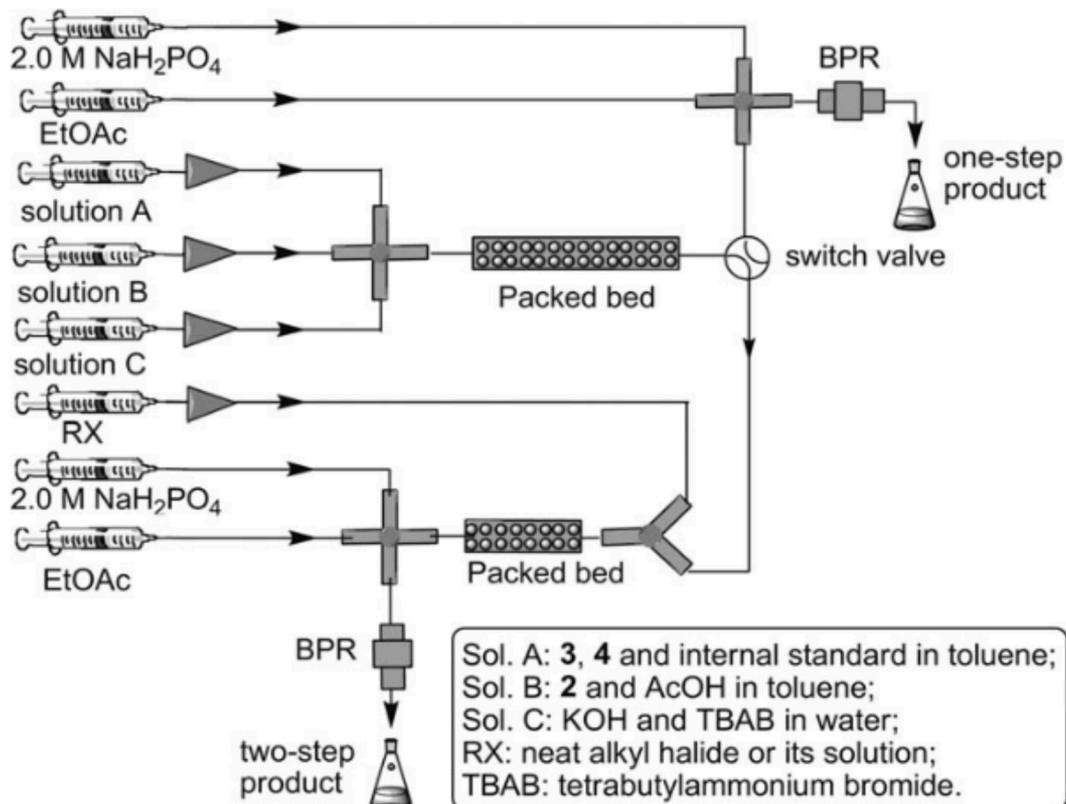
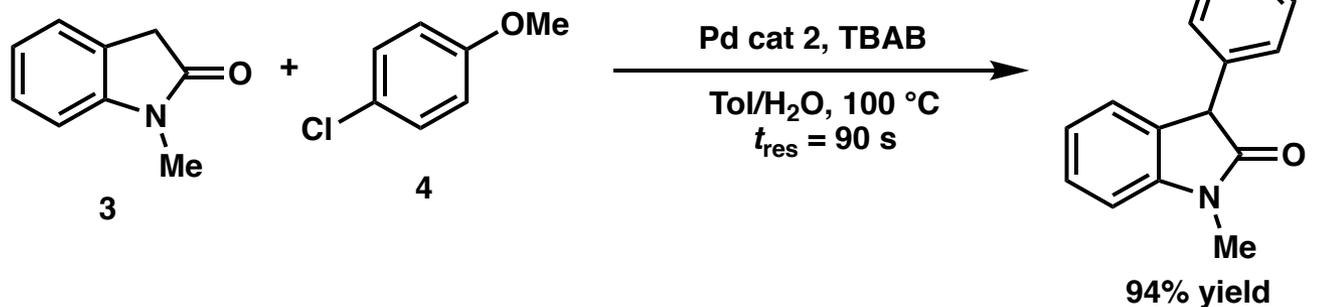


| entry | Pd Source (1 mol %)  | Base                    | Solvent              | Yield |
|-------|----------------------|-------------------------|----------------------|-------|
| 1     | Pd(dba) <sub>2</sub> | KHMDS                   | THF/Tol              | <5    |
| 2     | Pd(dba) <sub>2</sub> | LiMHDS                  | THF/Tol              | 12    |
| 3     | 2                    | LiHMDS                  | THF/Tol              | 5     |
| 4     | 2                    | 2.0 M KOH<br>*with TBAB | Tol/H <sub>2</sub> O | 91    |

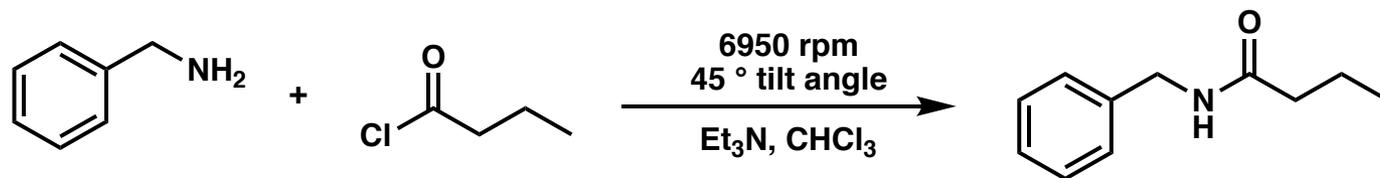
rapid/efficient mixing is crucial for high yields!



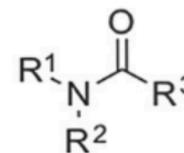
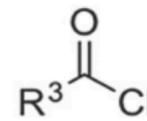
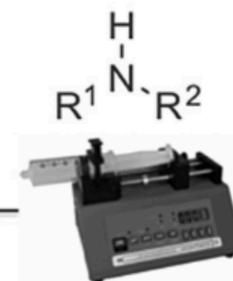
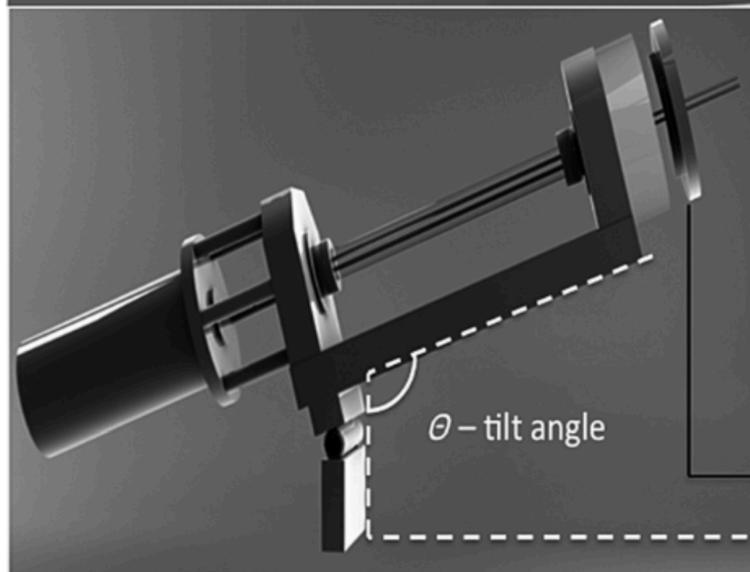
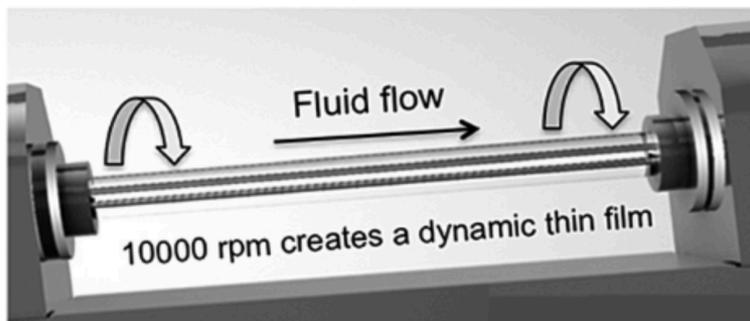
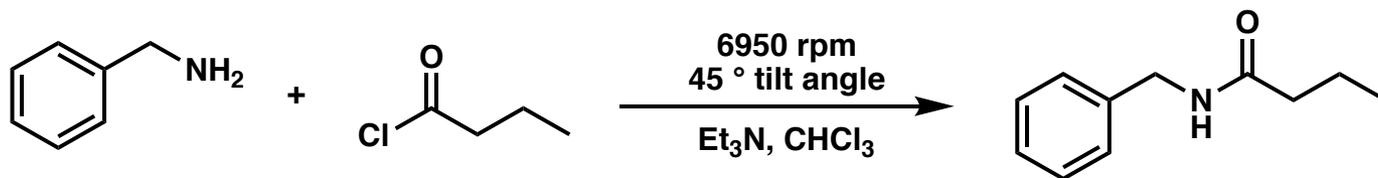
# Packed-Bed Reactor



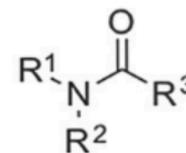
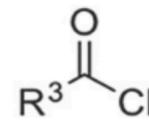
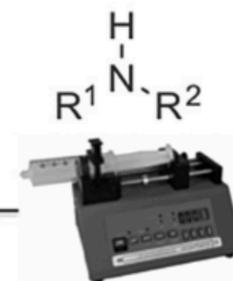
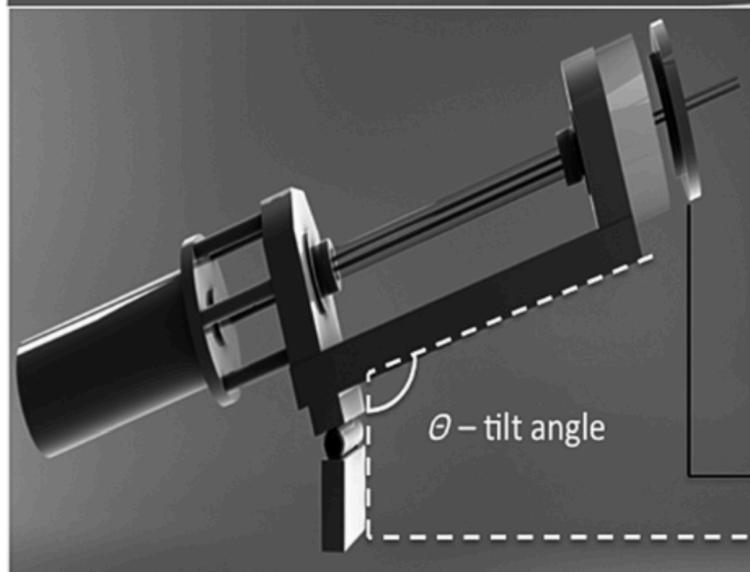
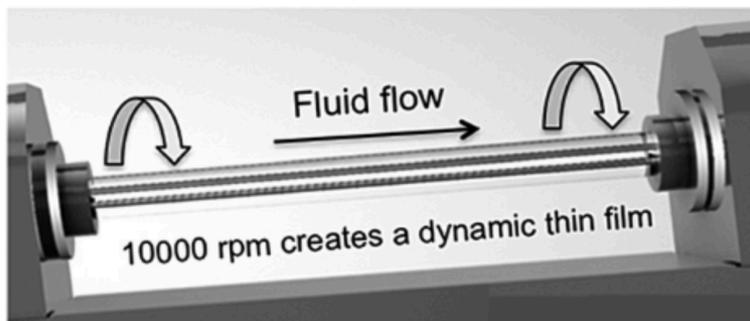
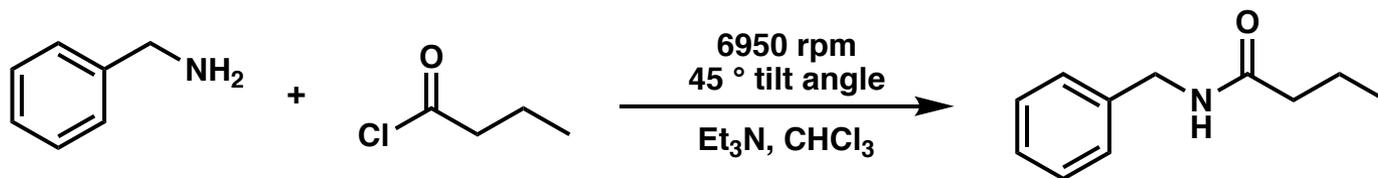
## *Rapid Vortex Fluidics*



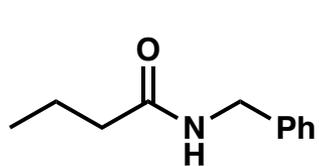
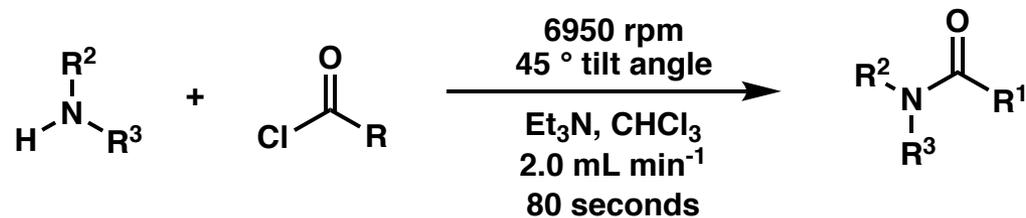
# Rapid Vortex Fluidics



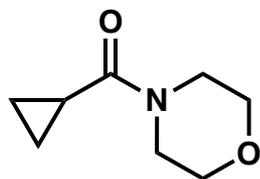
# Rapid Vortex Fluidics



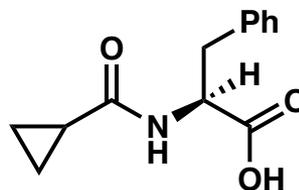
# Rapid Vortex Fluidics



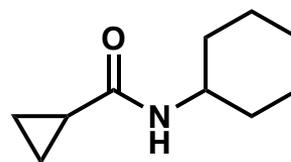
95% yield



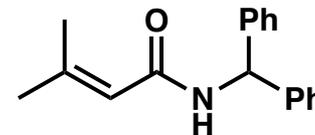
95% yield



99% yield

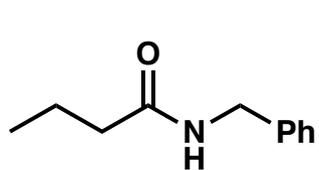
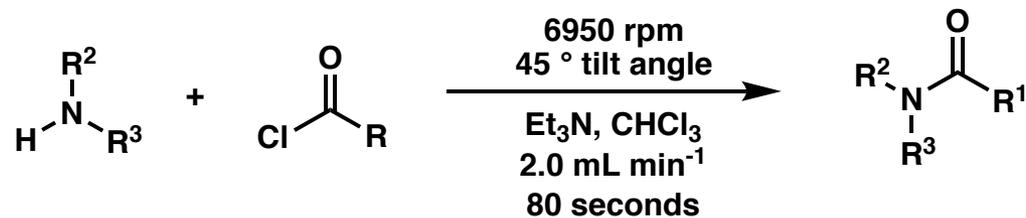


91% yield

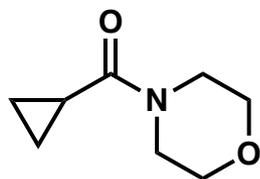


88% yield

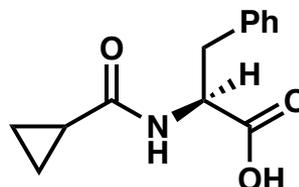
# Rapid Vortex Fluidics



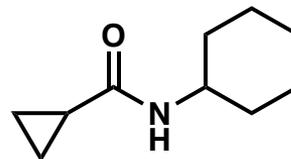
95% yield



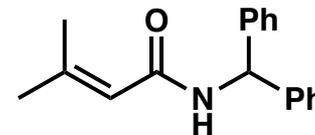
95% yield



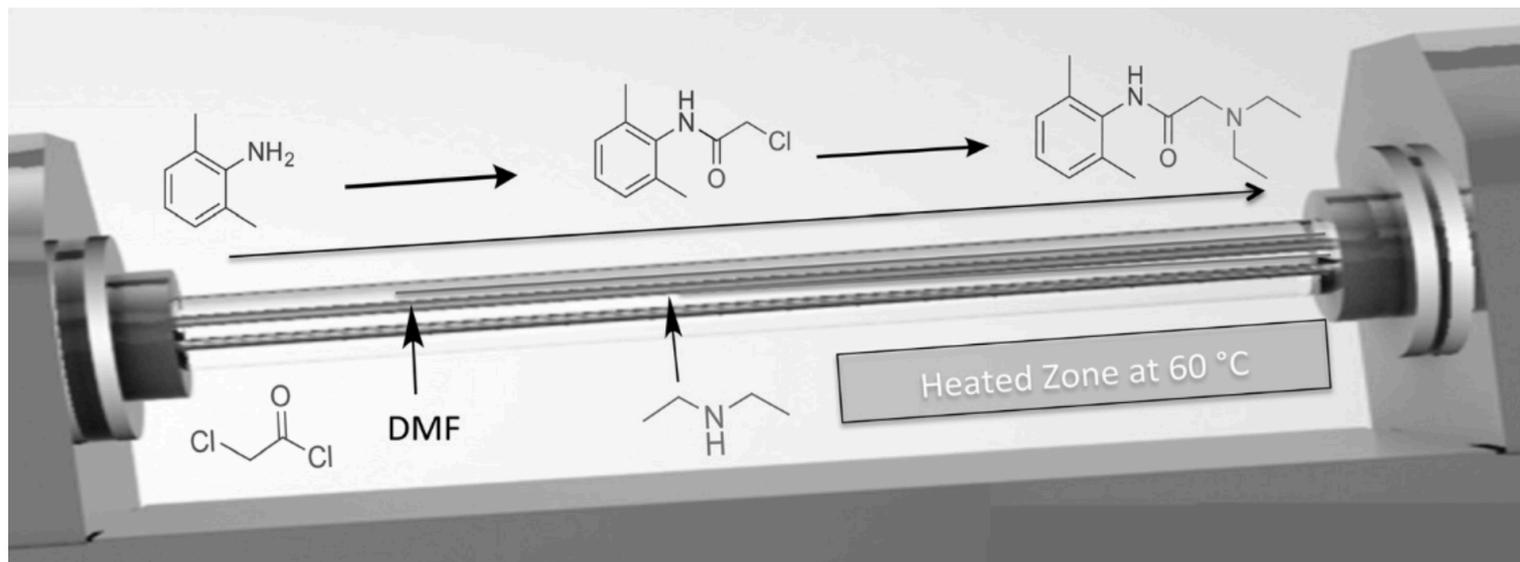
99% yield



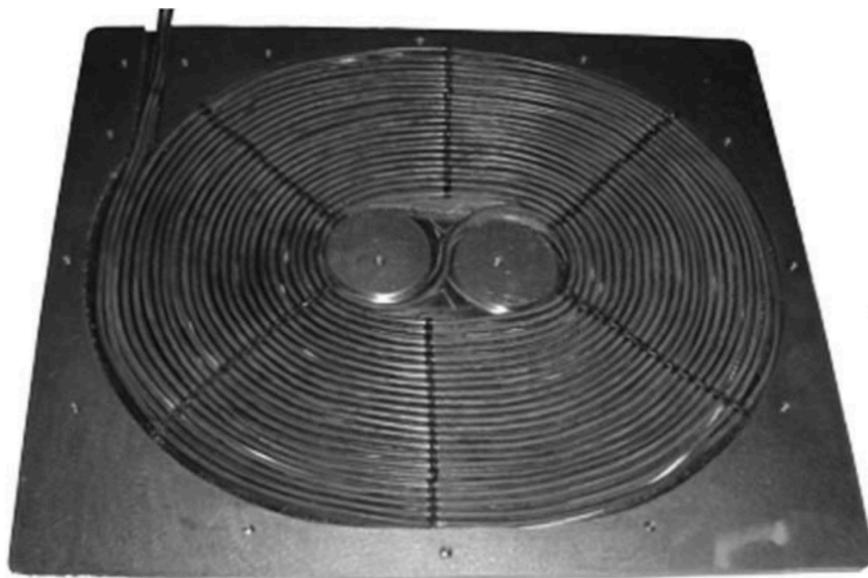
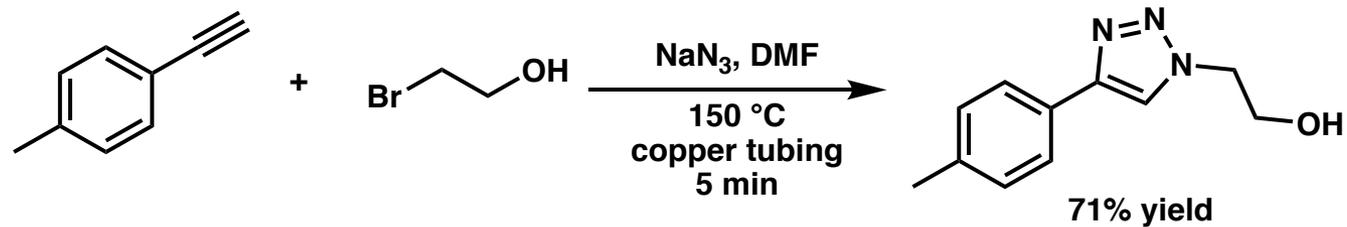
91% yield



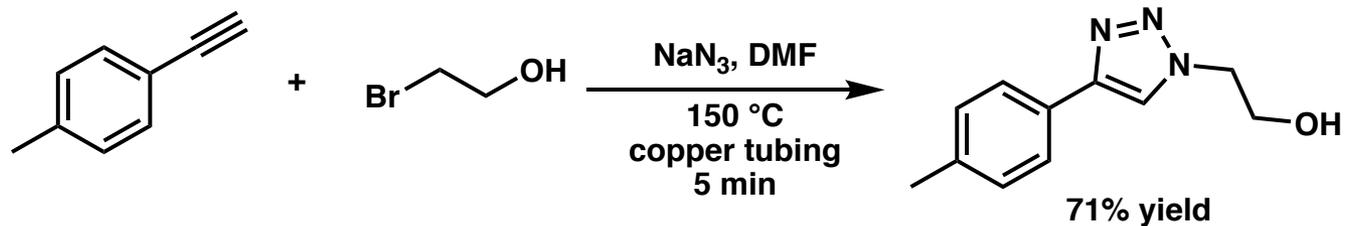
88% yield



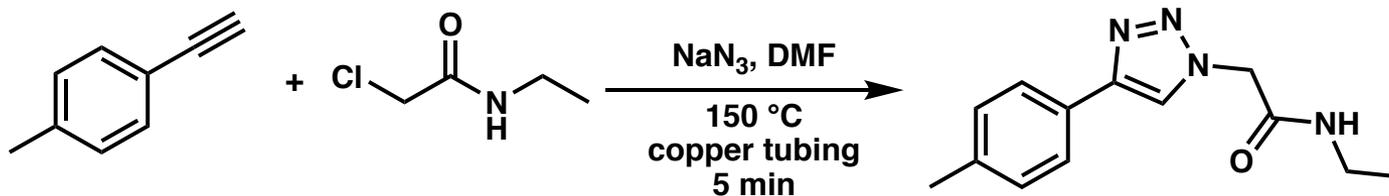
## Copper-Tube Reactor



## Copper-Tube Reactor

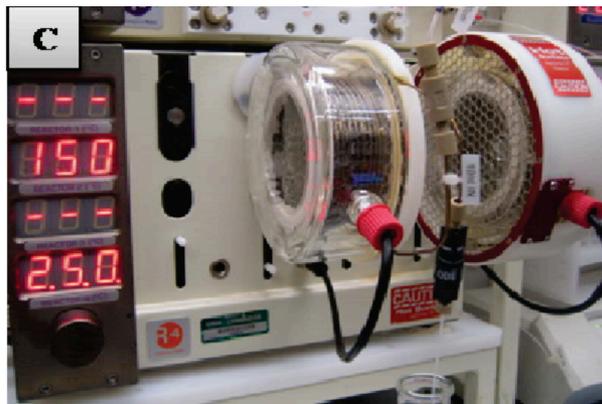
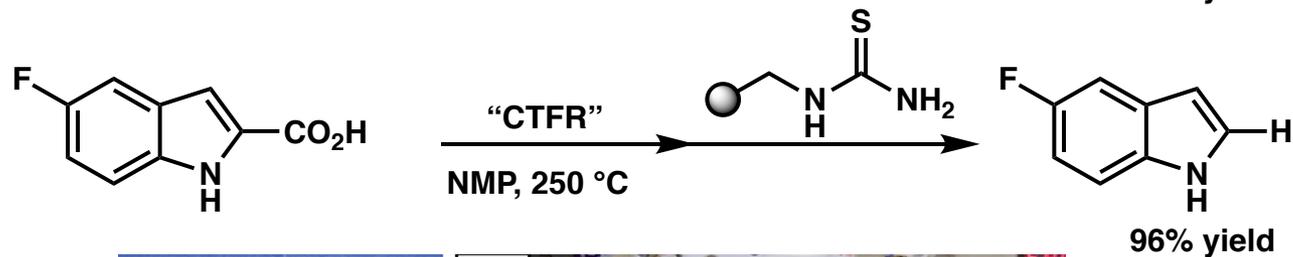
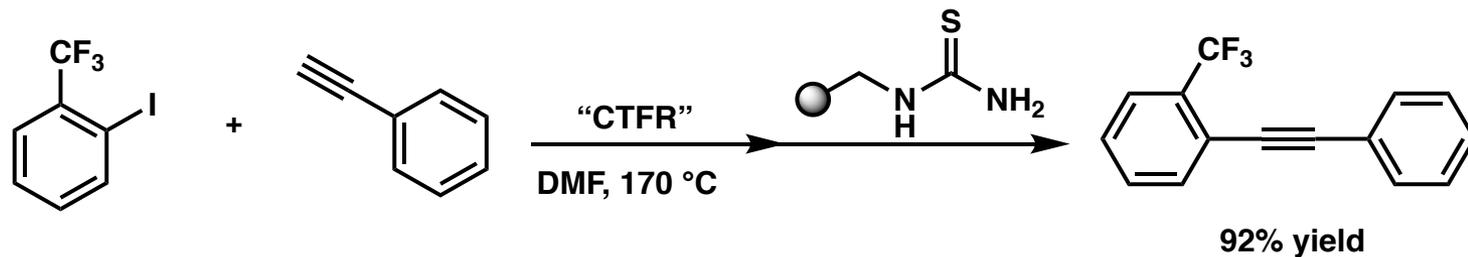
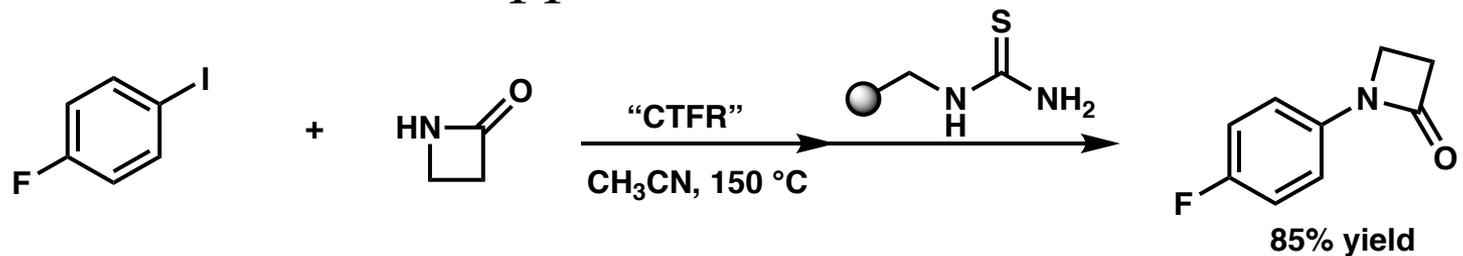


30 different triazoles prepared in a couple hours

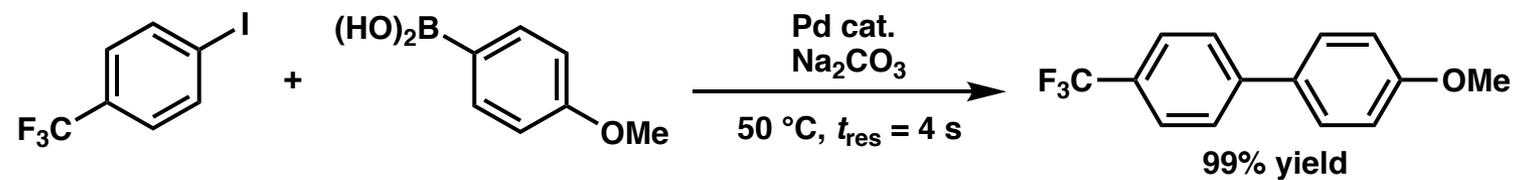


| <u>time</u> | <u>output</u> |
|-------------|---------------|
| 12 min      | 115 mg        |
| 1 hour      | 575 mg        |
| 1 day       | 13.8 g        |

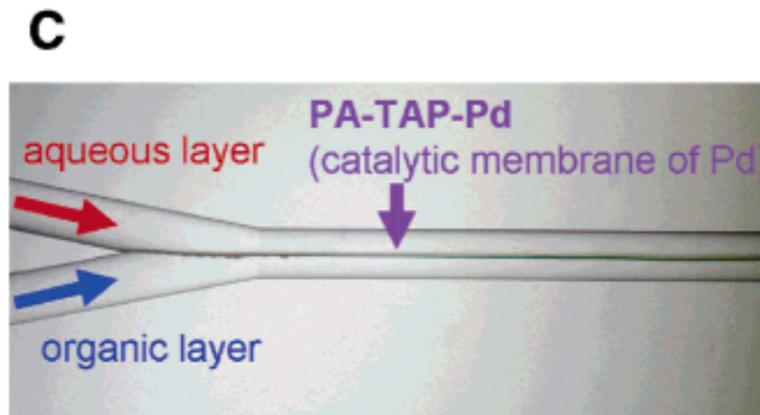
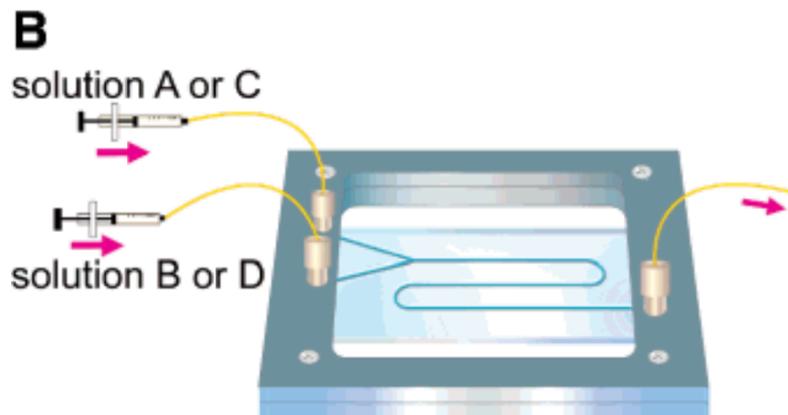
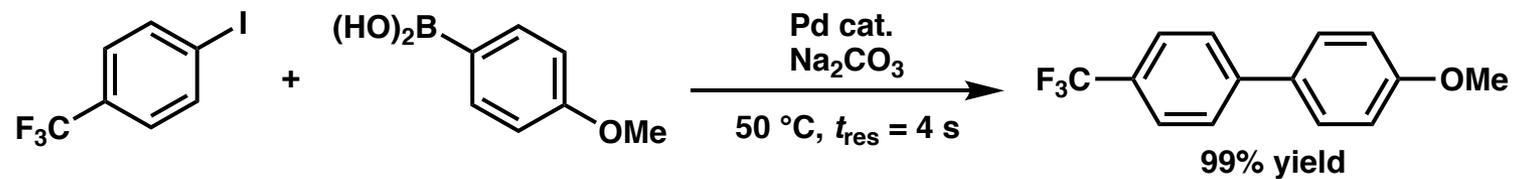
# Copper-Tube Reactor



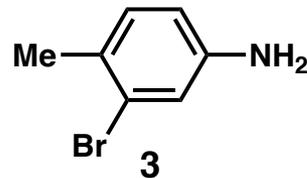
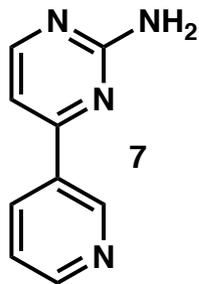
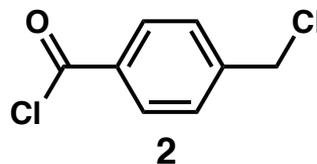
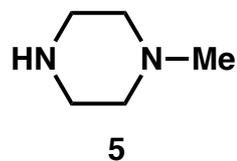
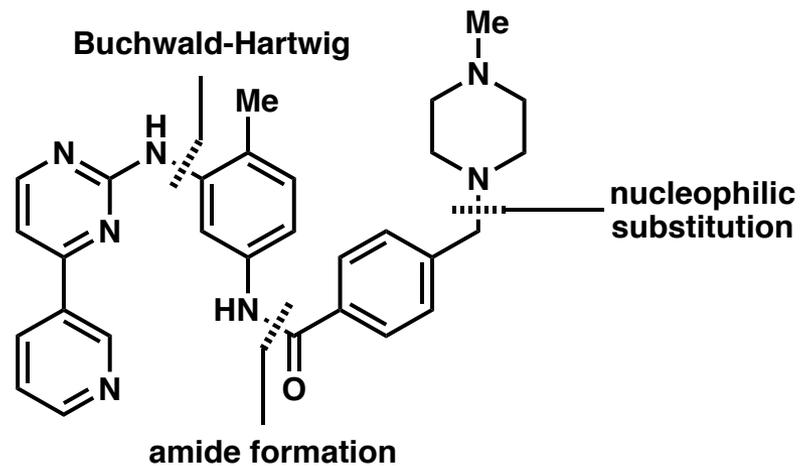
## Cross-Coupling in Flow



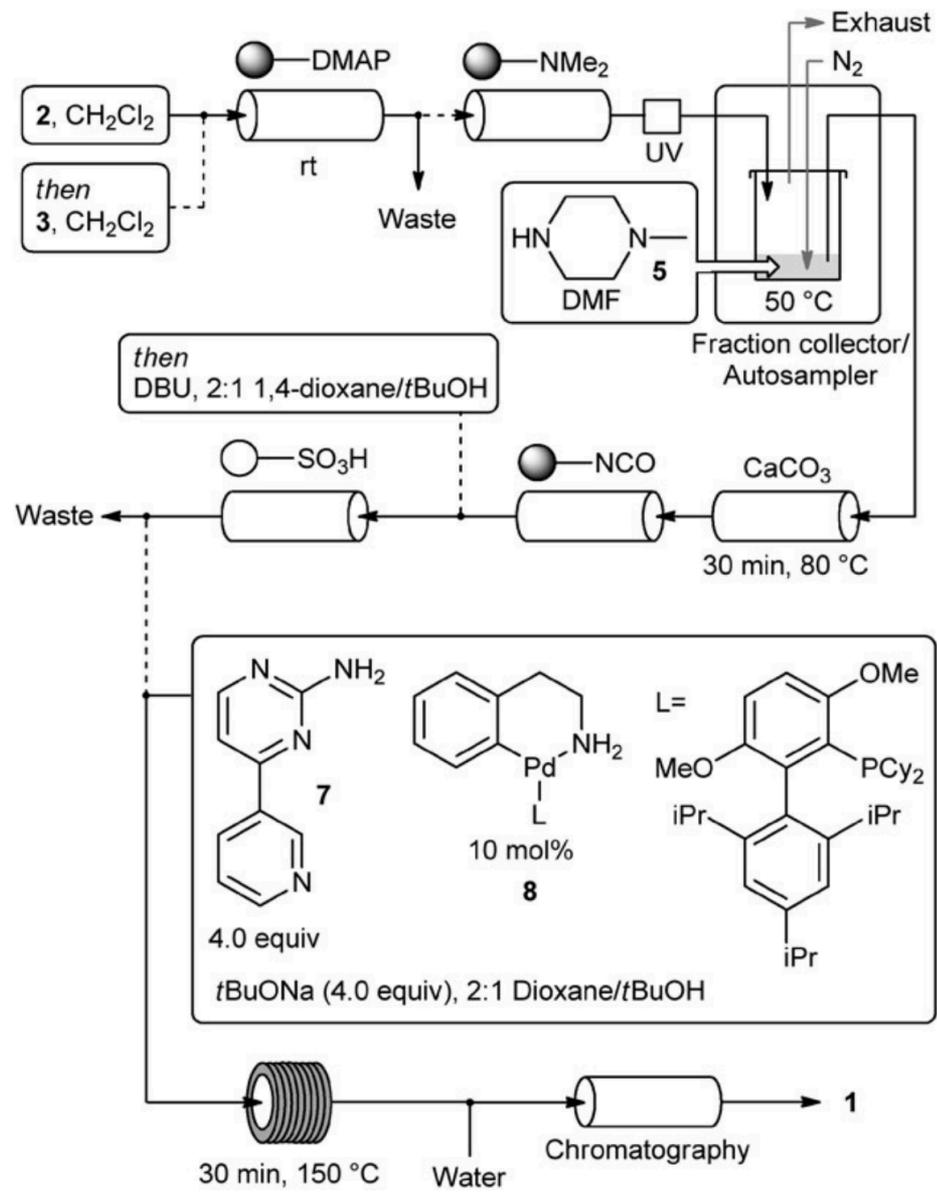
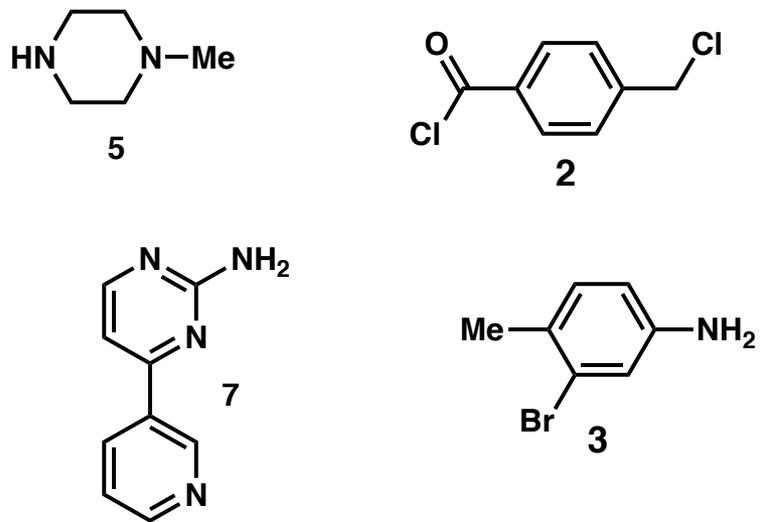
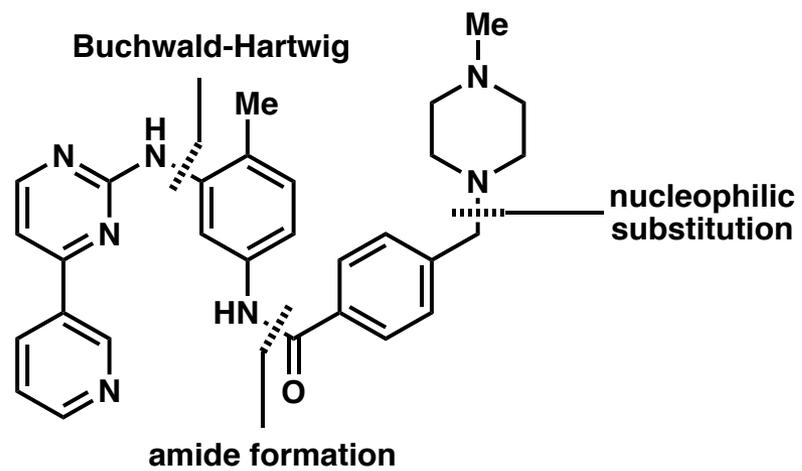
# Cross-Coupling in Flow



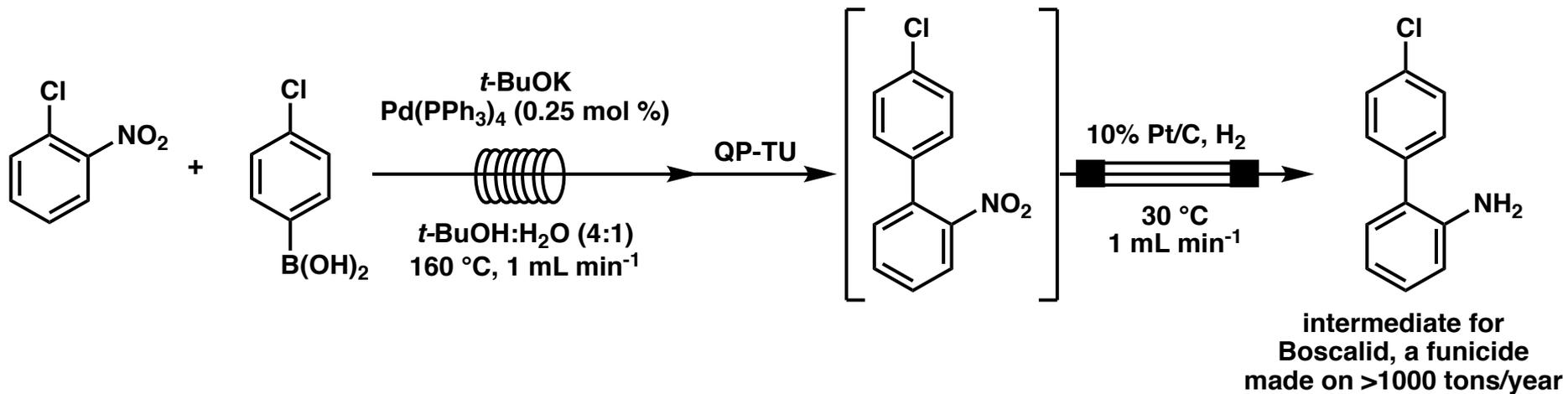
# Cross-Coupling in Flow: Synthesis of Imatinib



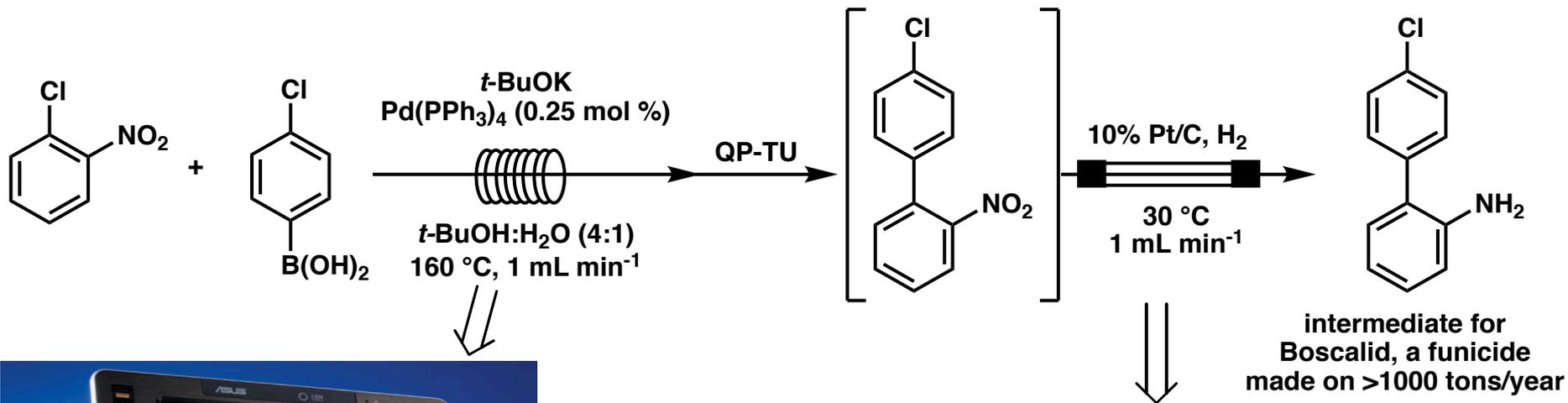
# Cross-Coupling in Flow: Synthesis of Imatinib



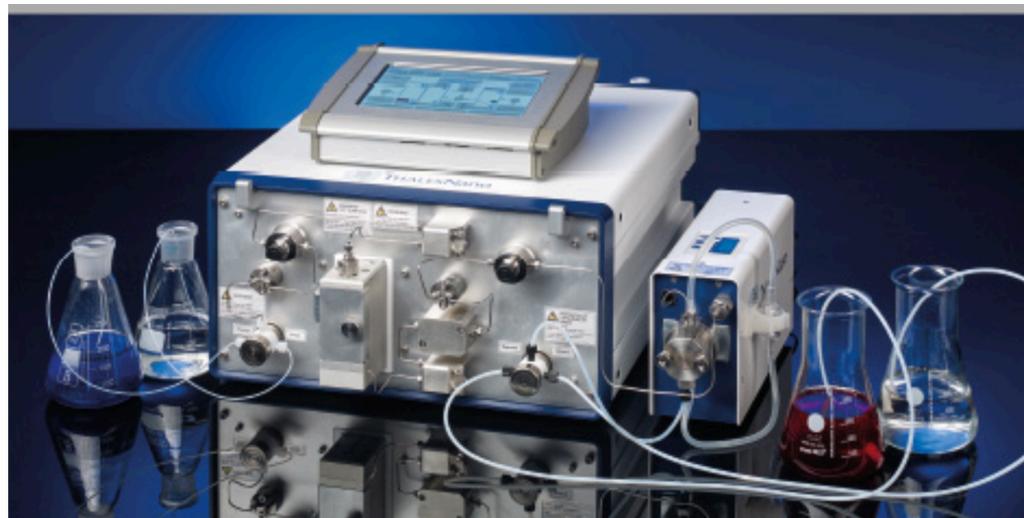
# Continuous Flow Hydrogenation (H-Cube)



# Continuous Flow Hydrogenation (H-Cube)

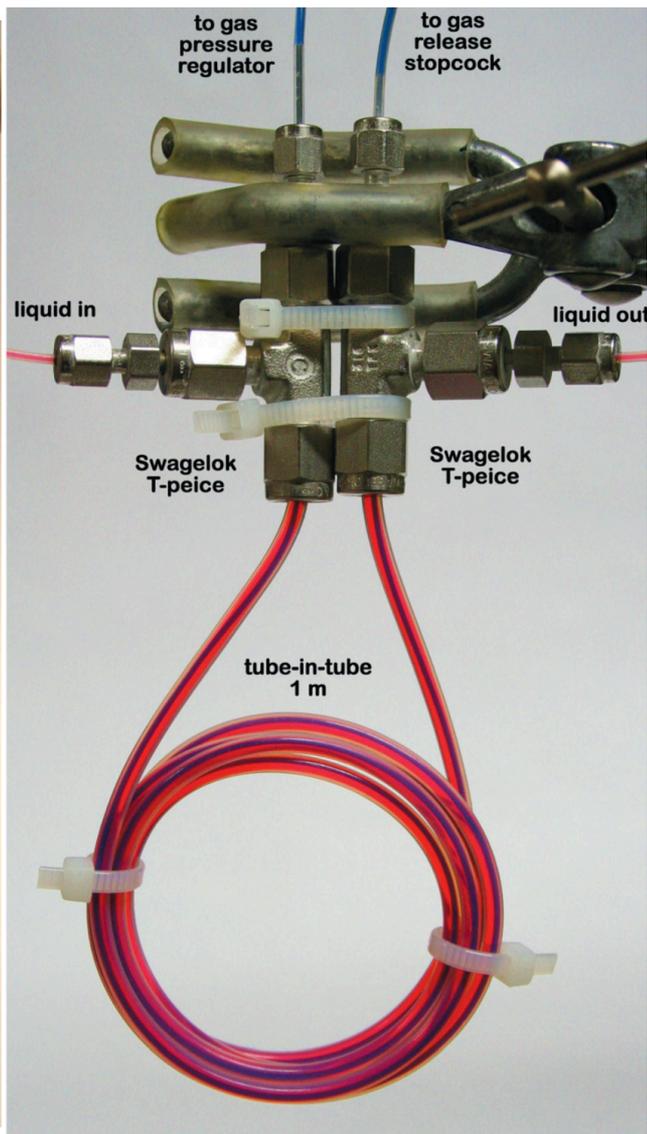
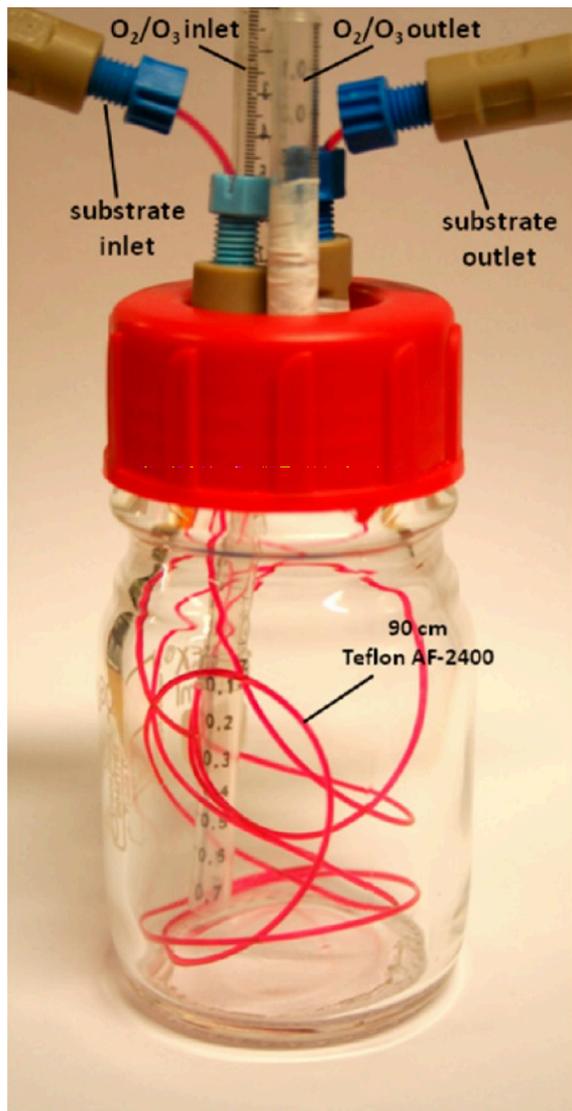


ThalesNano X-Cube



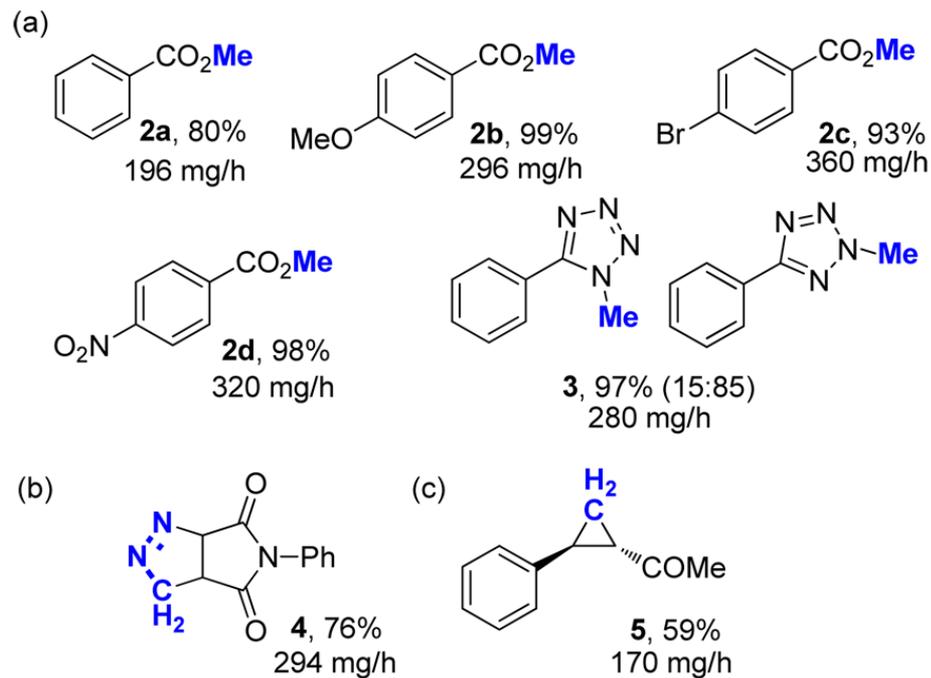
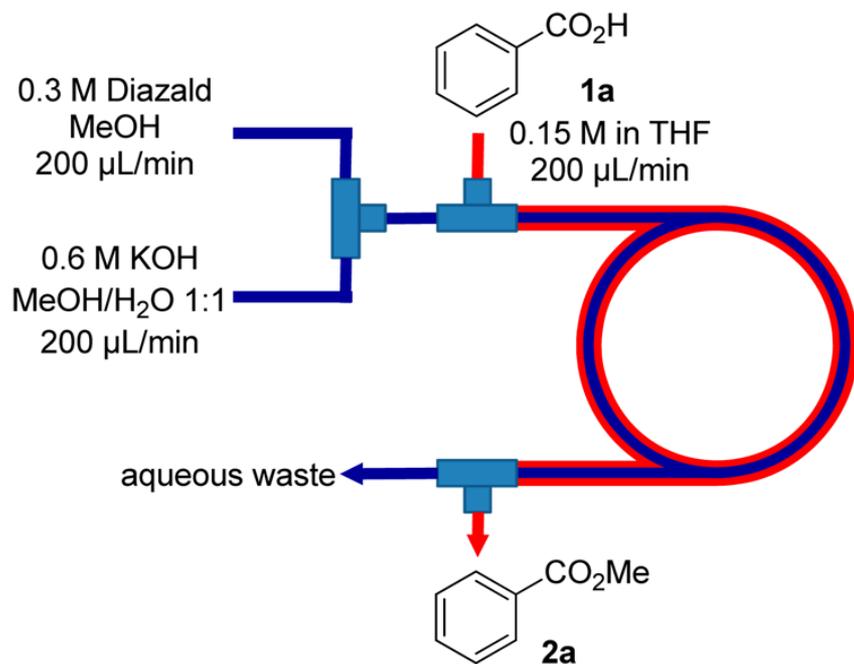
ThalesNano H-Cube

# Gas-Liquid Transformations with Tube-in-Tube Reactor

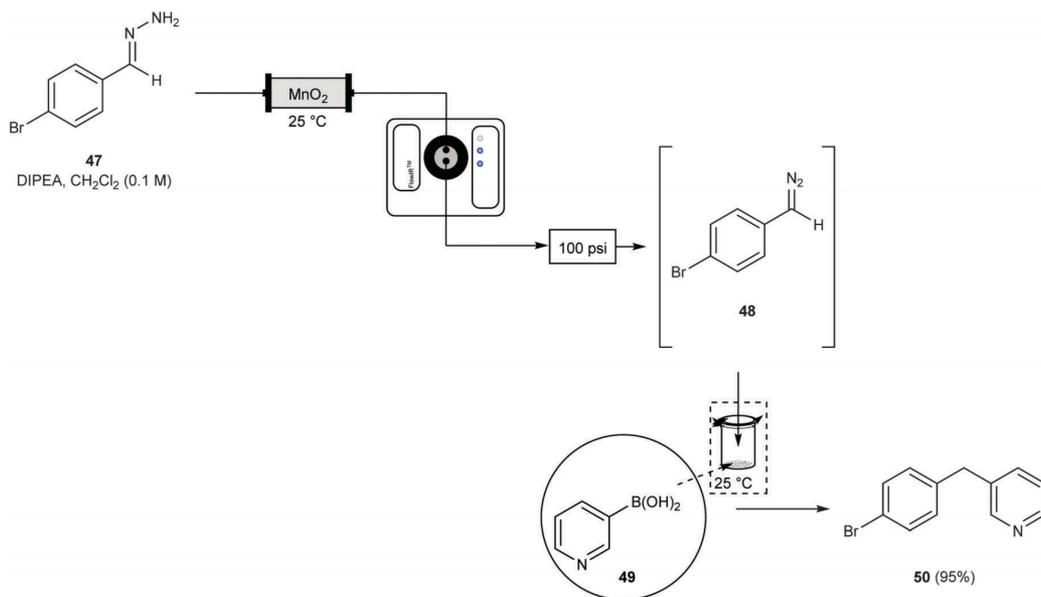
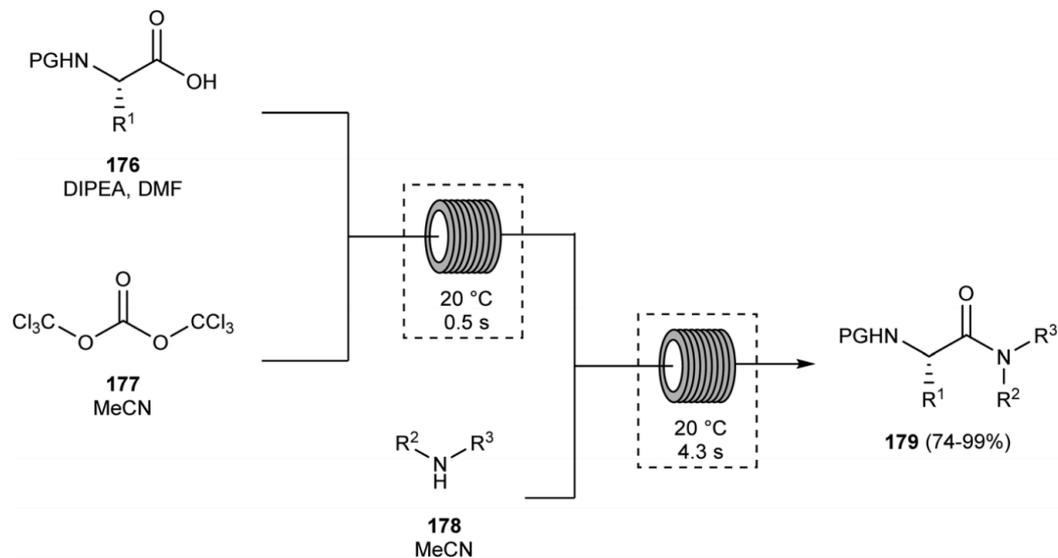


- CO<sub>2</sub> carboxylation of Grignards
- CO methoxycarboxylation
- Me<sub>2</sub>NH/CO dimethylaminocarbonylation
- ethylene Heck-vinylation
- CO/H<sub>2</sub> hydroformylation
- NH<sub>3</sub> Paal-Knorr
- O<sub>2</sub> Wacker Oxidation

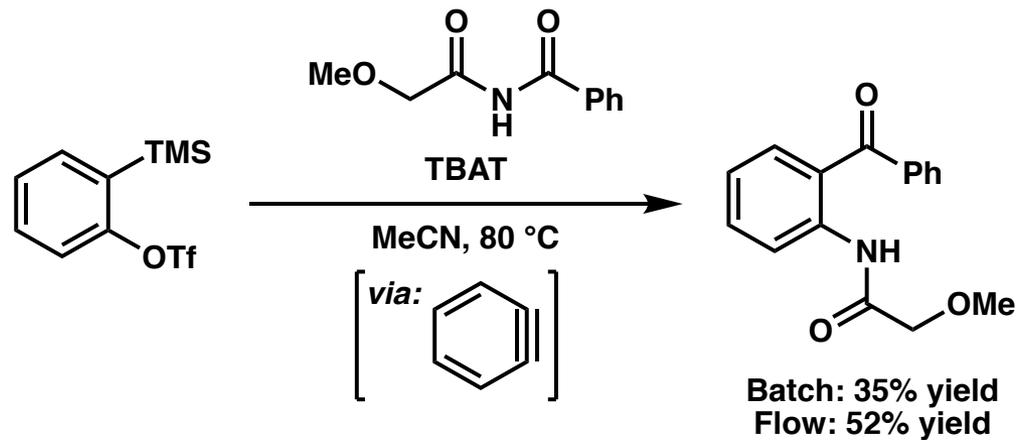
# Taming Hazardous Reagents Using Flow



# Taming Hazardous Reagents Using Flow

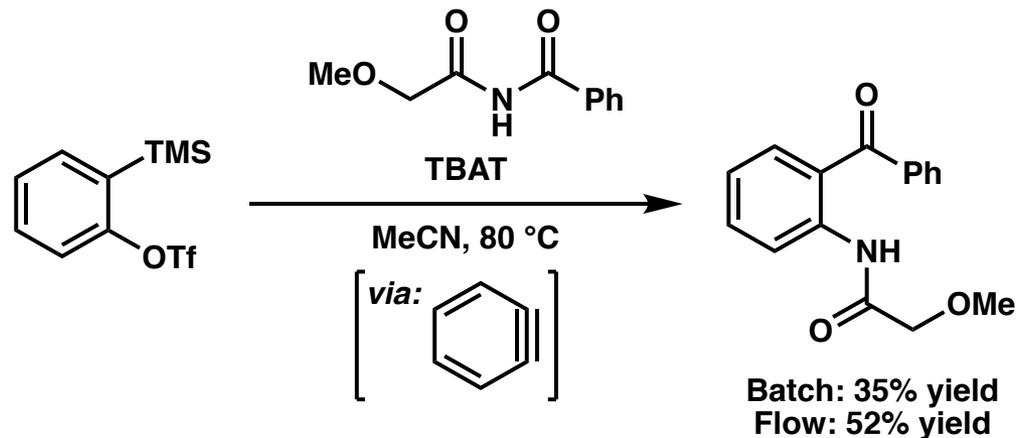


## Generation/Reaction of Arynes in Flow

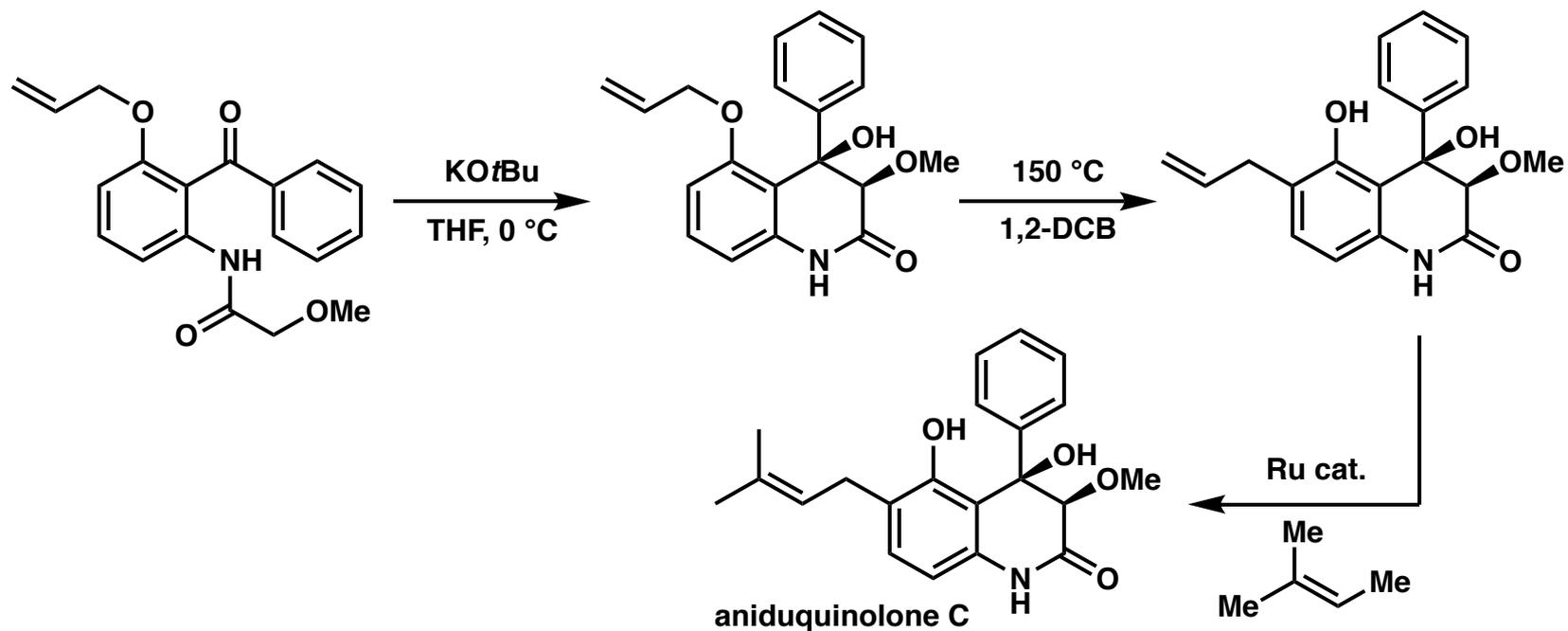


–increased mass/heat transfer in flow allows for highly reactive intermediates to react with higher selectivity

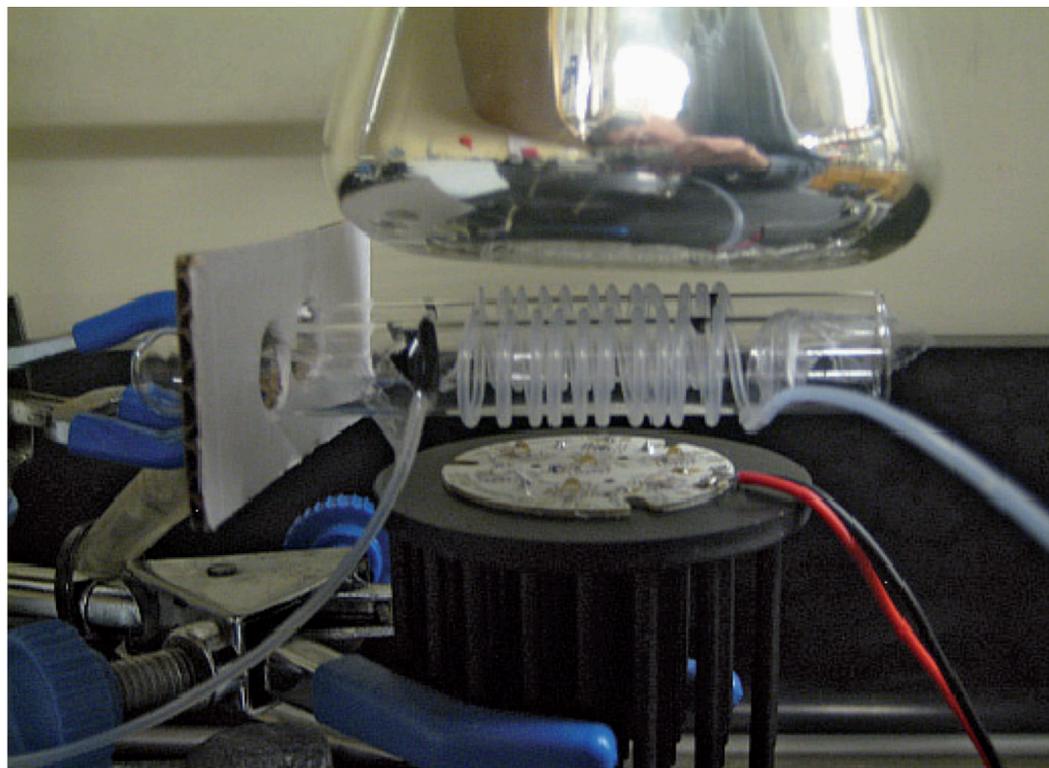
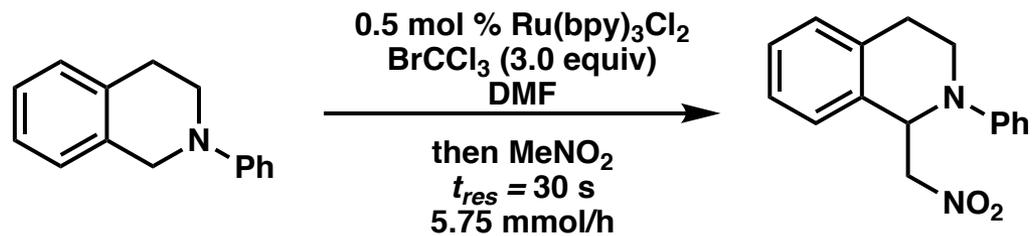
# Generation/Reaction of Arynes in Flow



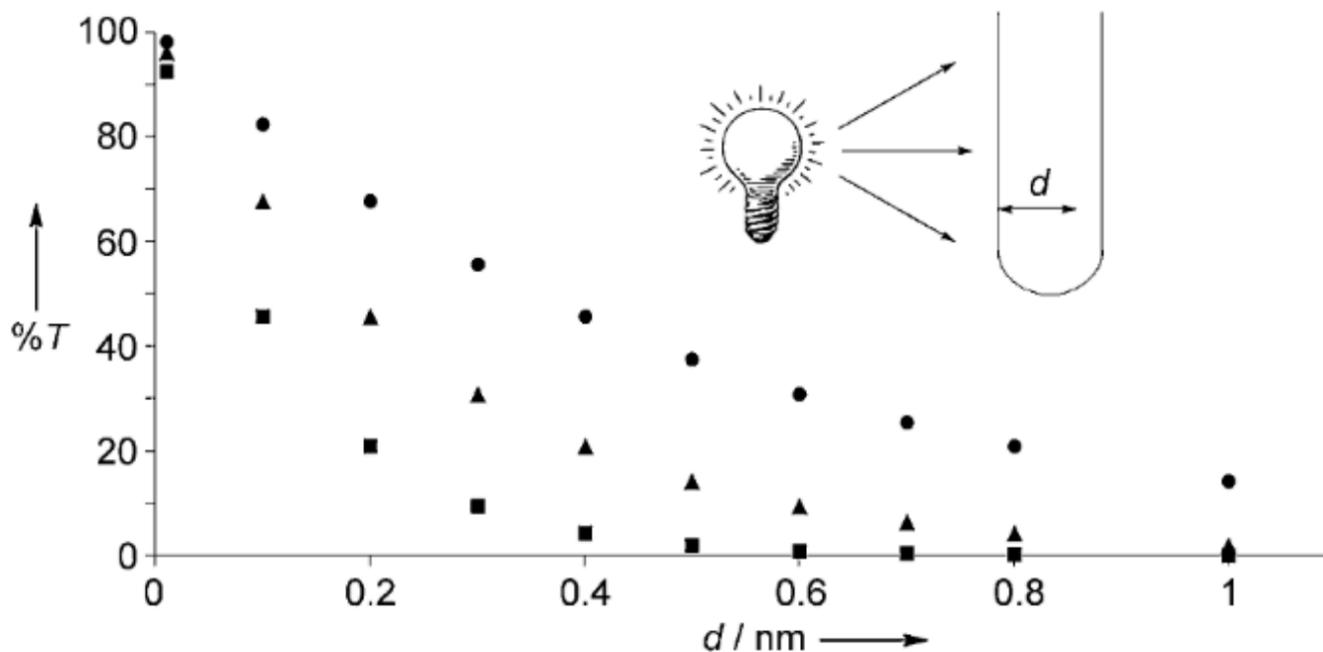
-increased mass/heat transfer in flow allows for highly reactive intermediates to react with higher selectivity



# Flow Photochemistry

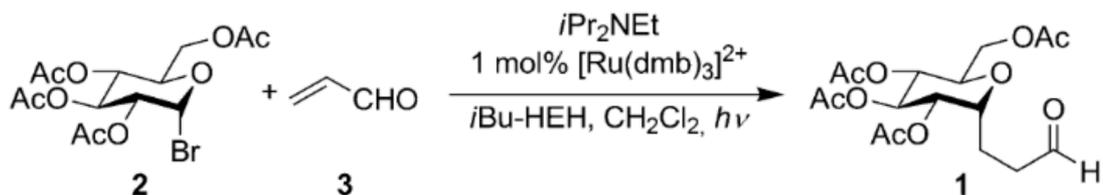


# Flow Photochemistry

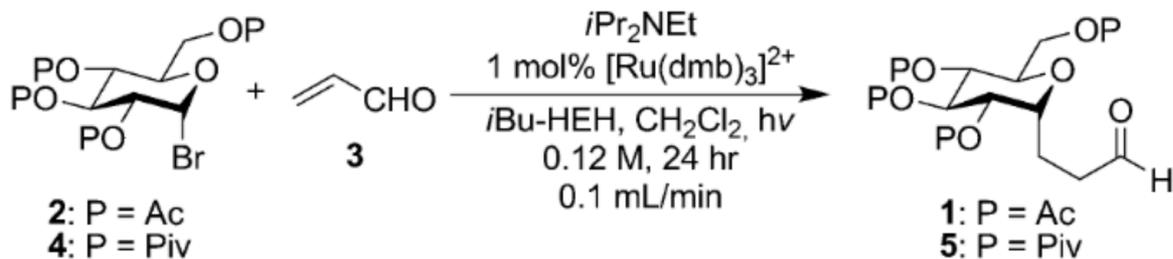


**Figure 1.** The percent transmittance versus distance from the wall ( $d$ ) as calculated from the Beer–Lambert law. ● 0.5 mM  $[\text{Ru}(\text{dmb})_3]^{2+}$ , ▲ 1 mM  $[\text{Ru}(\text{dmb})_3]^{2+}$ , ■ 2 mM  $[\text{Ru}(\text{dmb})_3]^{2+}$ .

# Flow Photochemistry

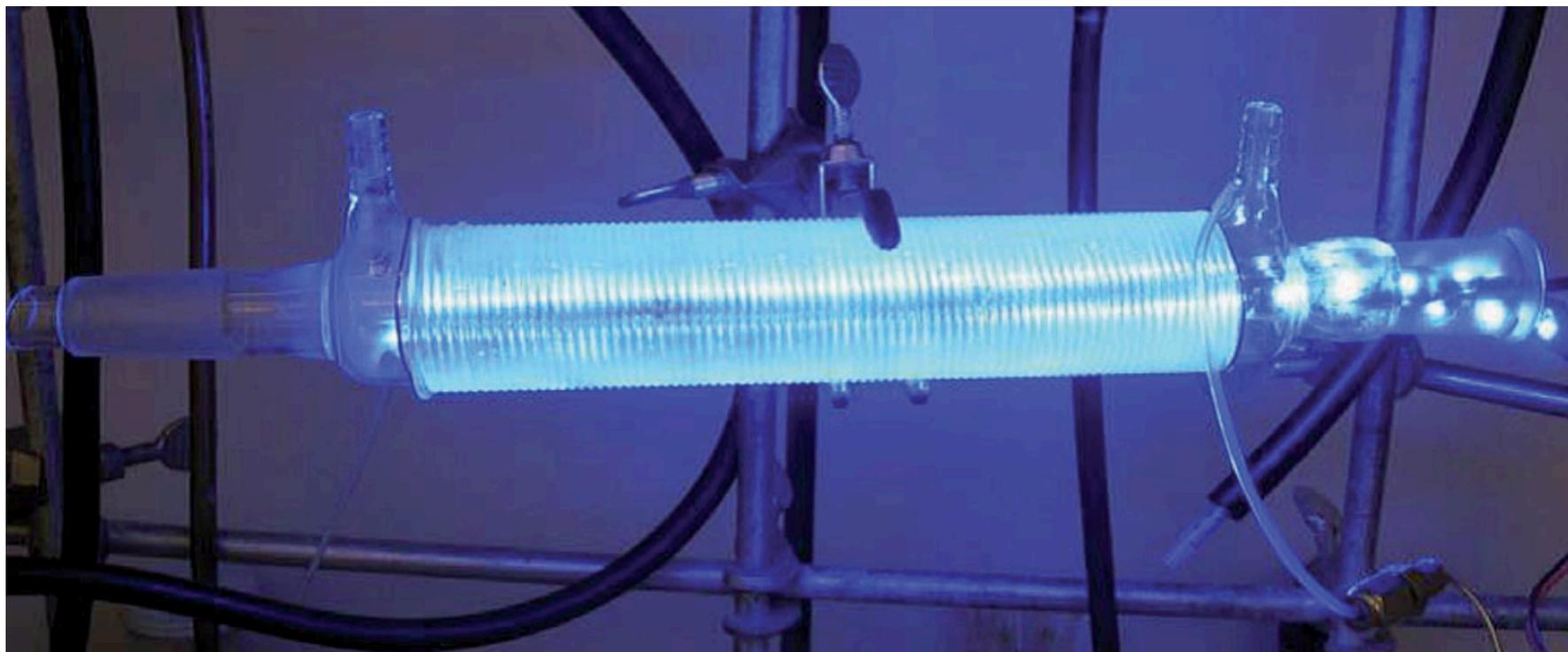


|               | $t$ [h] | <b>2</b> mmol | Conv. [%] | TOF [h <sup>-1</sup> ] |
|---------------|---------|---------------|-----------|------------------------|
| 25 mL flask   | 24      | 2.43          | 85        | 3.5                    |
| 5 mm NMR tube | 1       | 0.06          | 73        | 70                     |



**85% yield**  
**5.5 g**

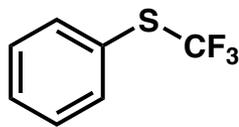
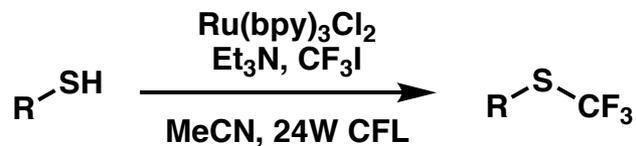
# *Flow Photochemistry*



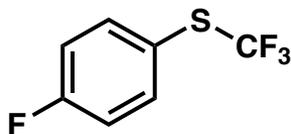
# *Flow Photochemistry*



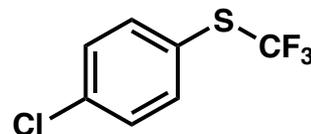
# Flow Photochemistry



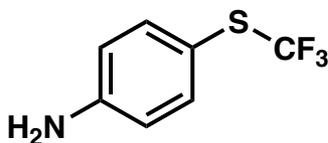
Batch: 30 min, 95% yield  
Flow: 1 min, 98% yield



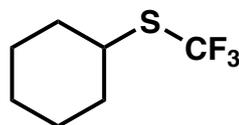
Batch: 2 h, 65% yield  
Flow: 1 min, 91% yield



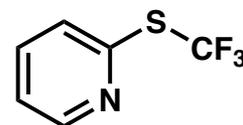
Batch: 1 h, 78% yield  
Flow: 1 min, 96% yield



Batch: 1.5 h, 88% yield  
Flow: 1 min, 73% yield

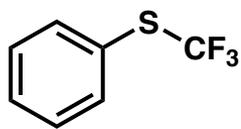
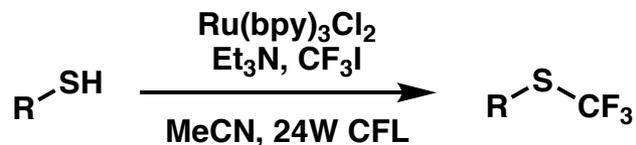


Batch: 2.5 h, 41% yield  
Flow: 30 min, 59% yield

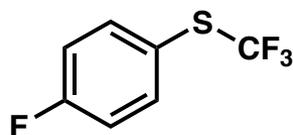


Batch: 1 h, 91% yield  
Flow: 1 min, 91% yield

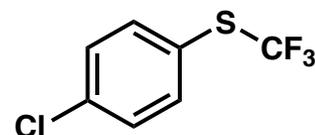
# Flow Photochemistry



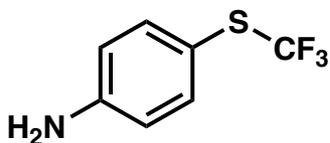
Batch: 30 min, 95% yield  
Flow: 1 min, 98% yield



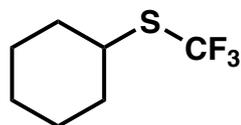
Batch: 2 h, 65% yield  
Flow: 1 min, 91% yield



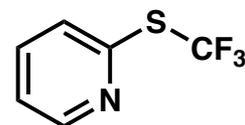
Batch: 1 h, 78% yield  
Flow: 1 min, 96% yield



Batch: 1.5 h, 88% yield  
Flow: 1 min, 73% yield



Batch: 2.5 h, 41% yield  
Flow: 30 min, 59% yield

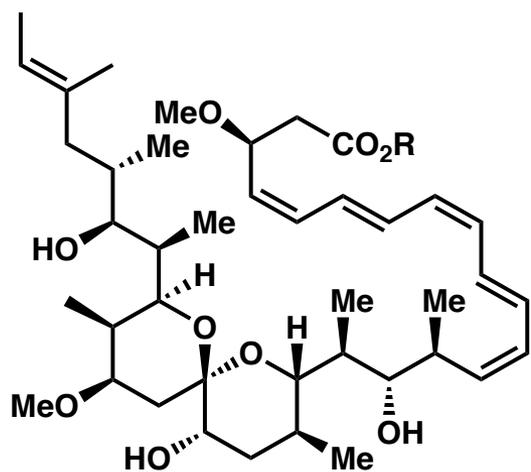


Batch: 1 h, 91% yield  
Flow: 1 min, 91% yield

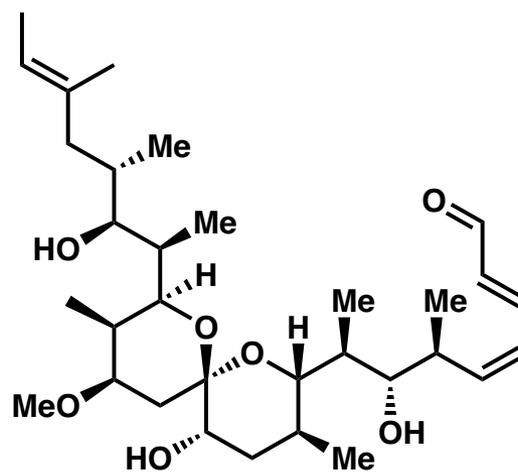
-segmented gas-liquid flow

-flow requires only 1.1 equiv of  $\text{CF}_3\text{I}$  (batch uses 4 equiv)

# Natural Product Total Synthesis Using Flow: Spirocyclic Polyketides

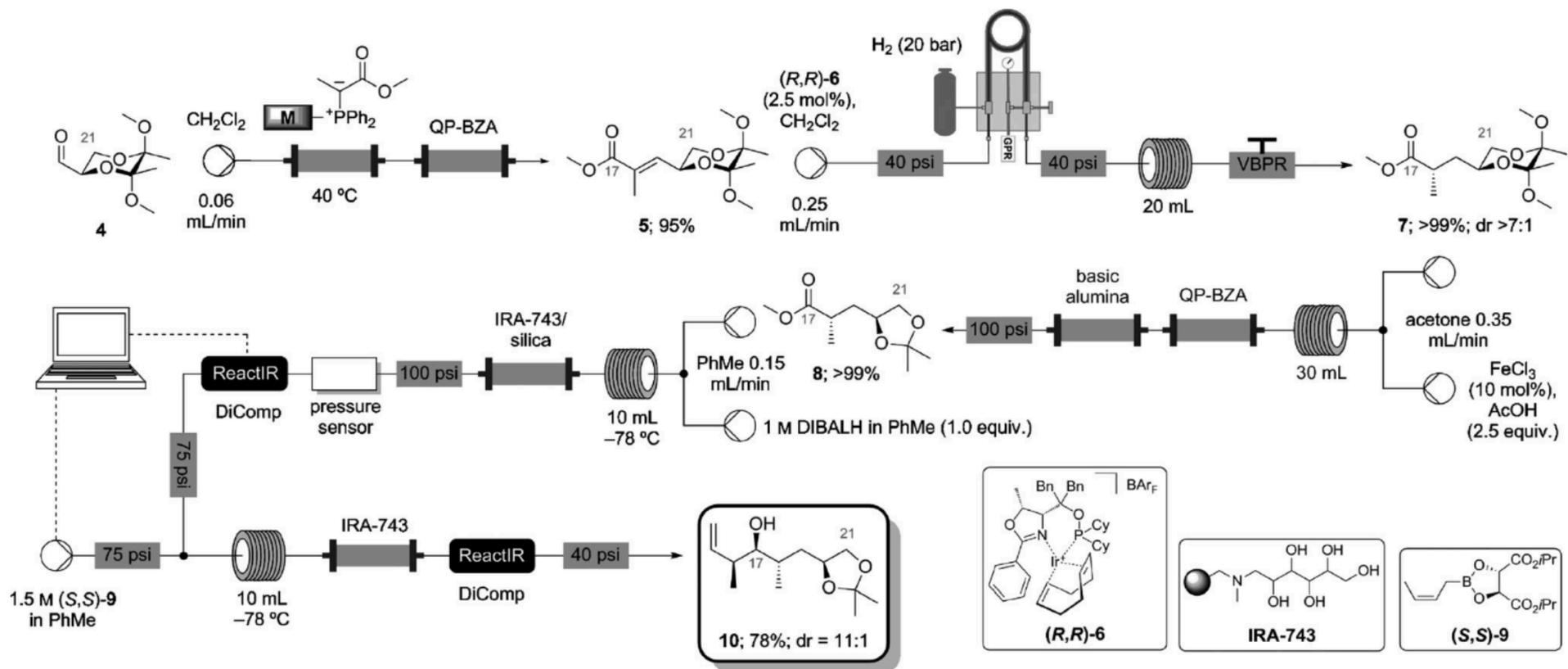


spirangien A (R = H)  
spirangien A methyl ester (R = Me)

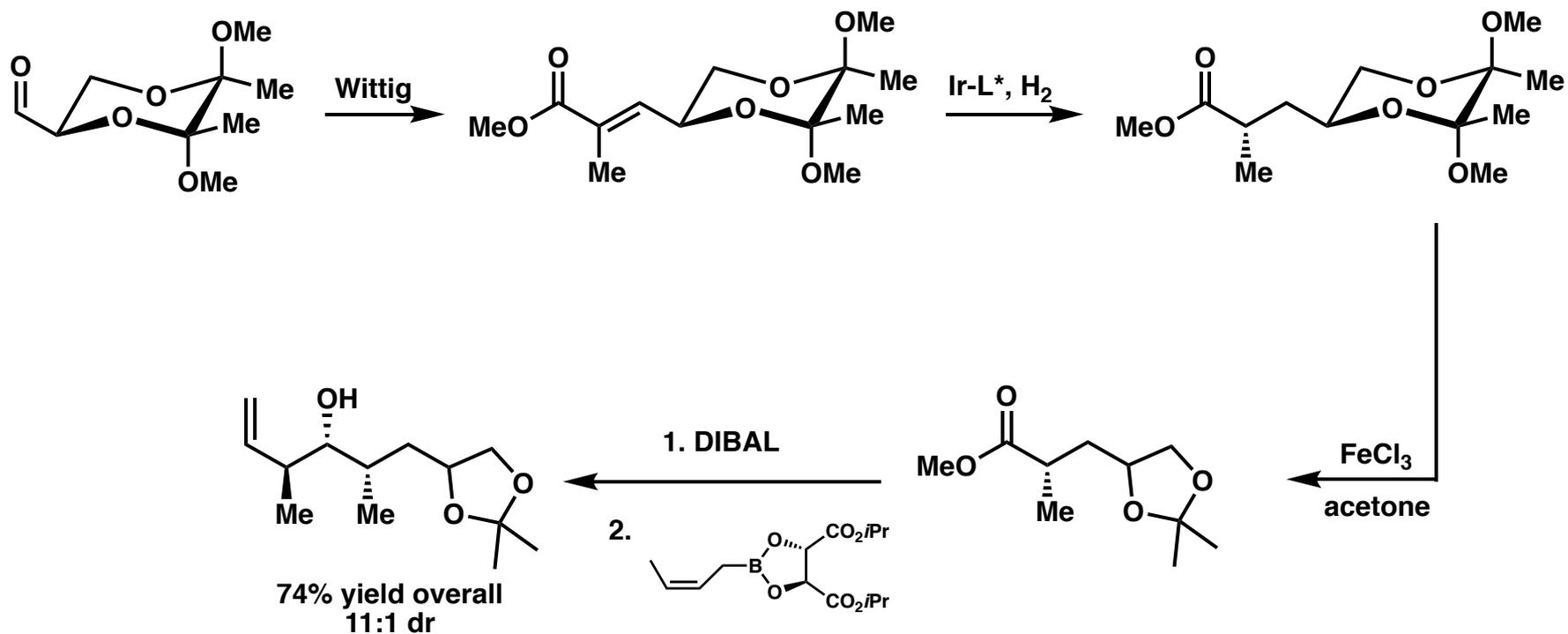


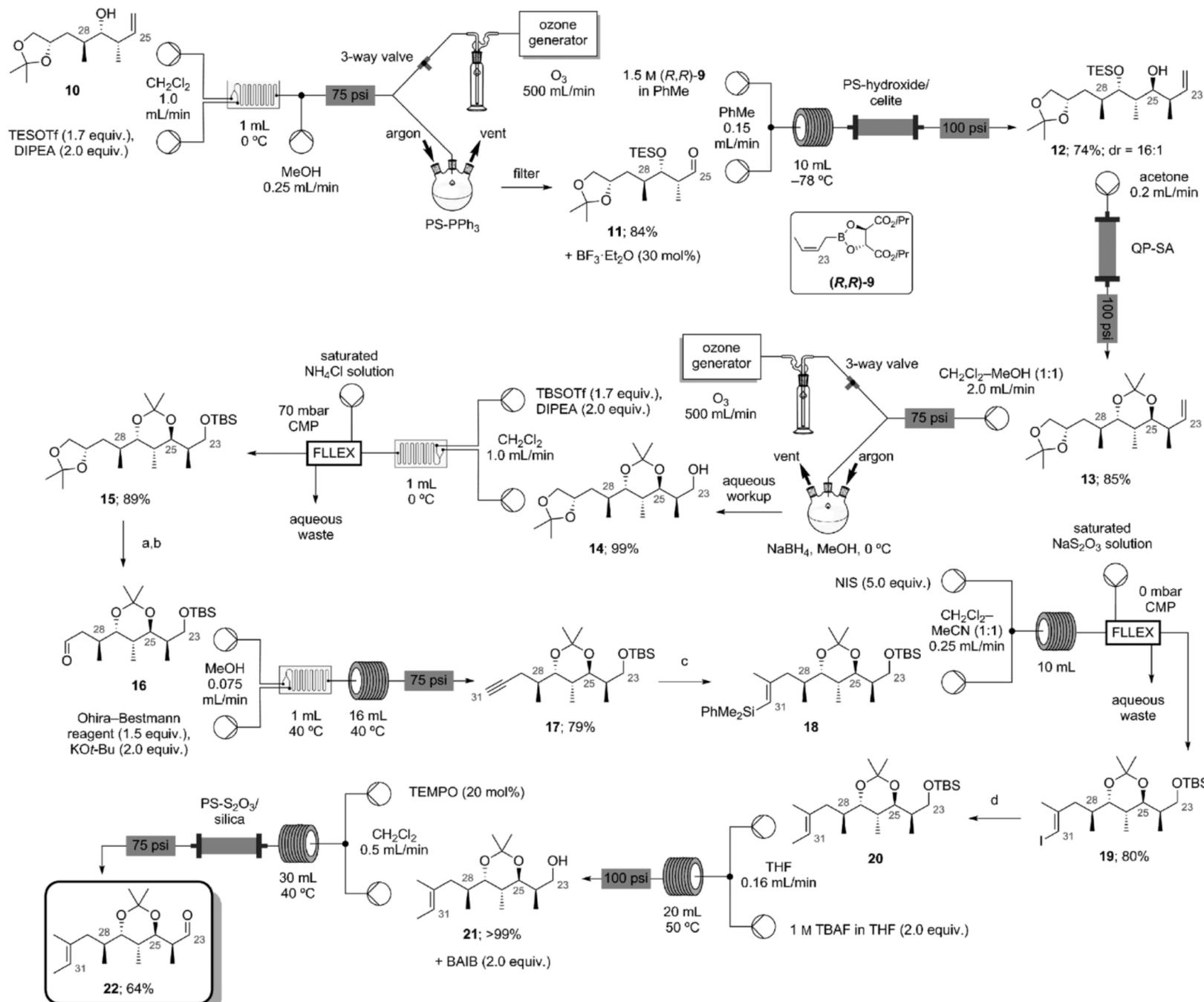
spirodienal A

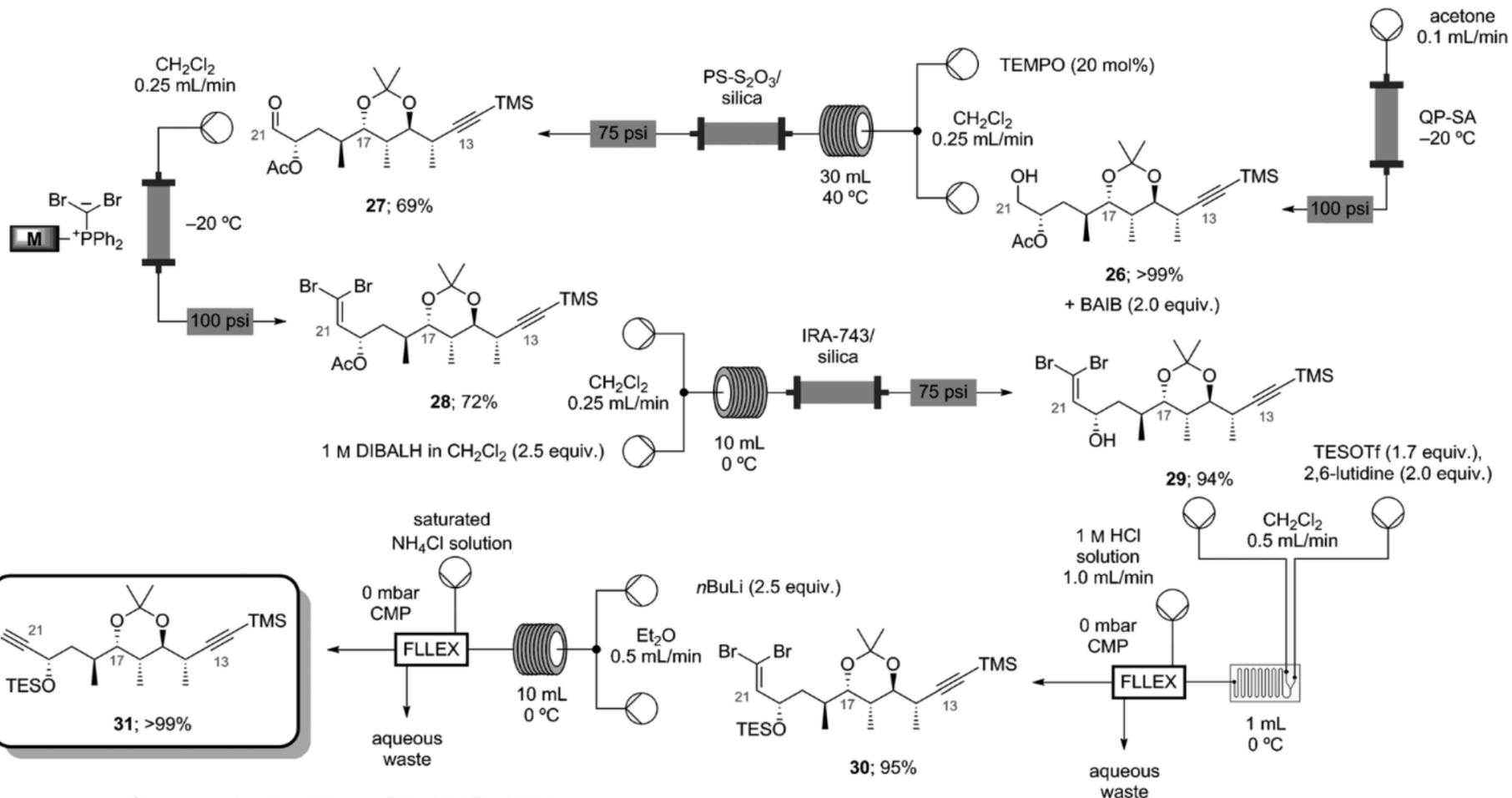
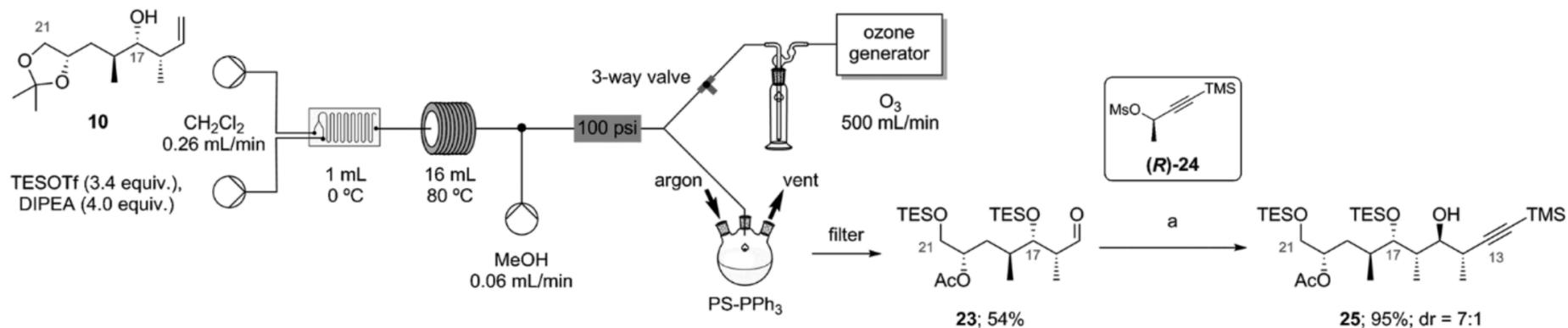
# Natural Product Total Synthesis Using Flow: Spirocyclic Polyketides



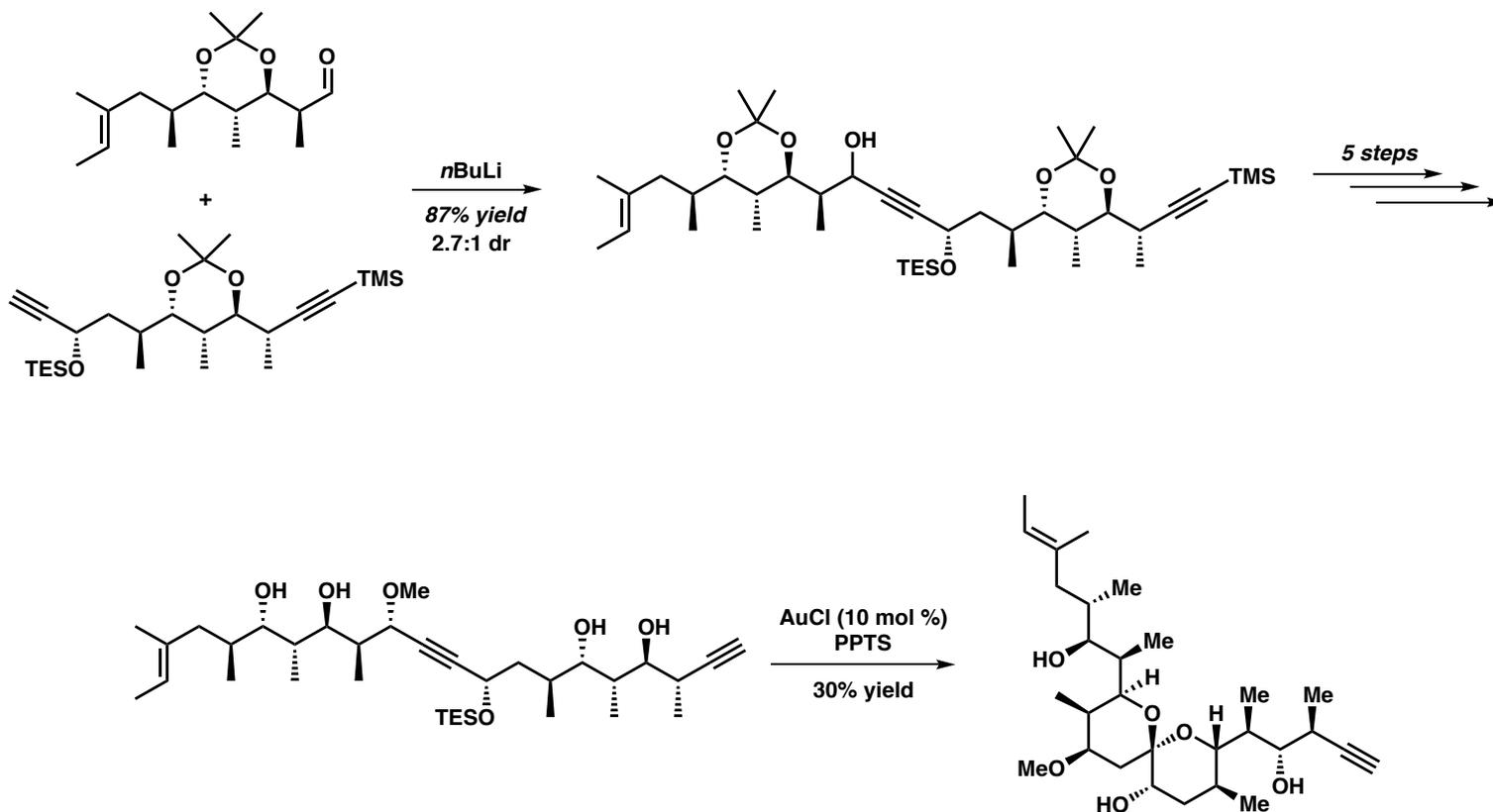
# Natural Product Total Synthesis Using Flow: Spirocyclic Polyketides



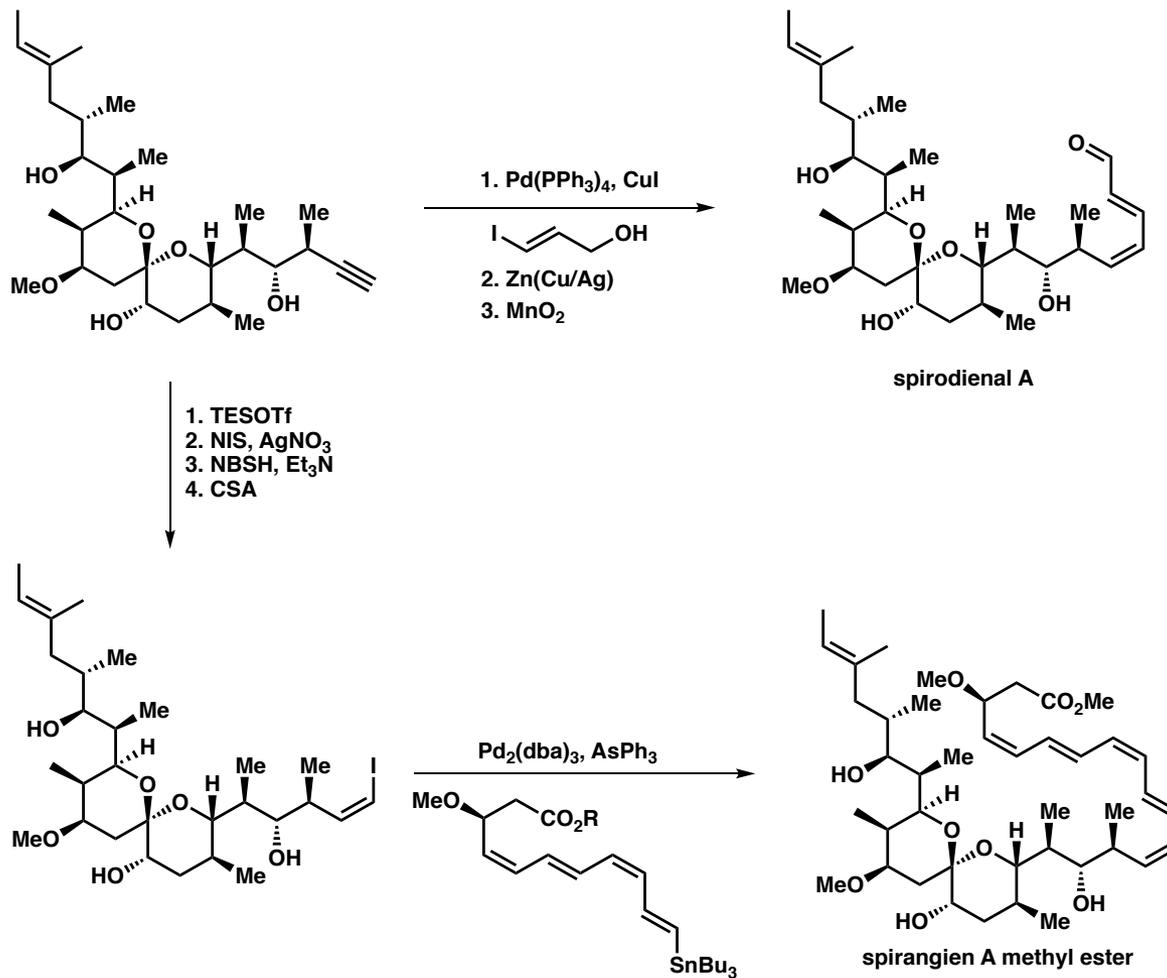




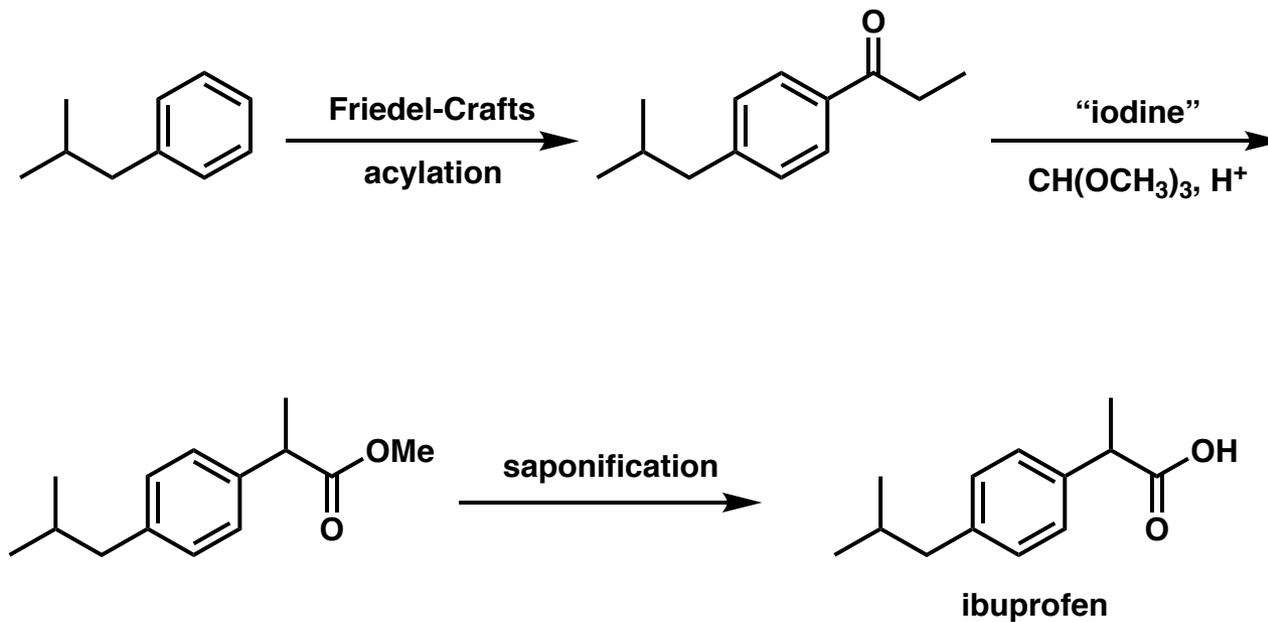
# Natural Product Total Synthesis Using Flow: Spirocyclic Polyketides



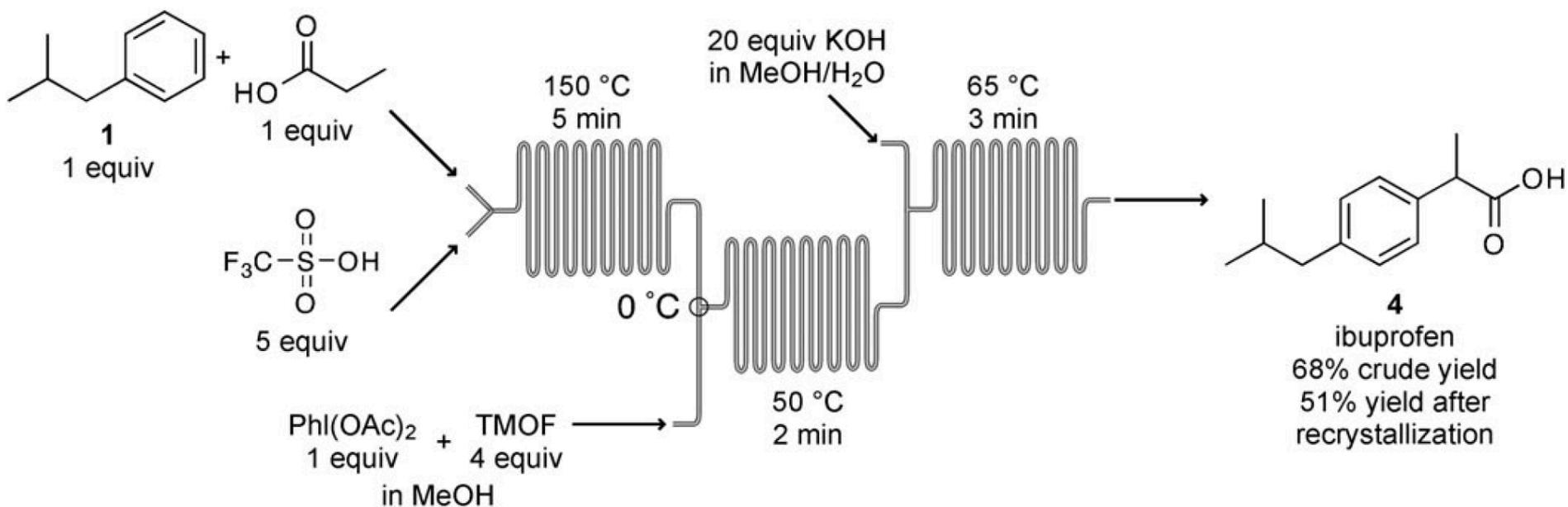
# Natural Product Total Synthesis Using Flow: Spirocyclic Polyketides



# Continuous Flow Synthesis of Ibuprofen

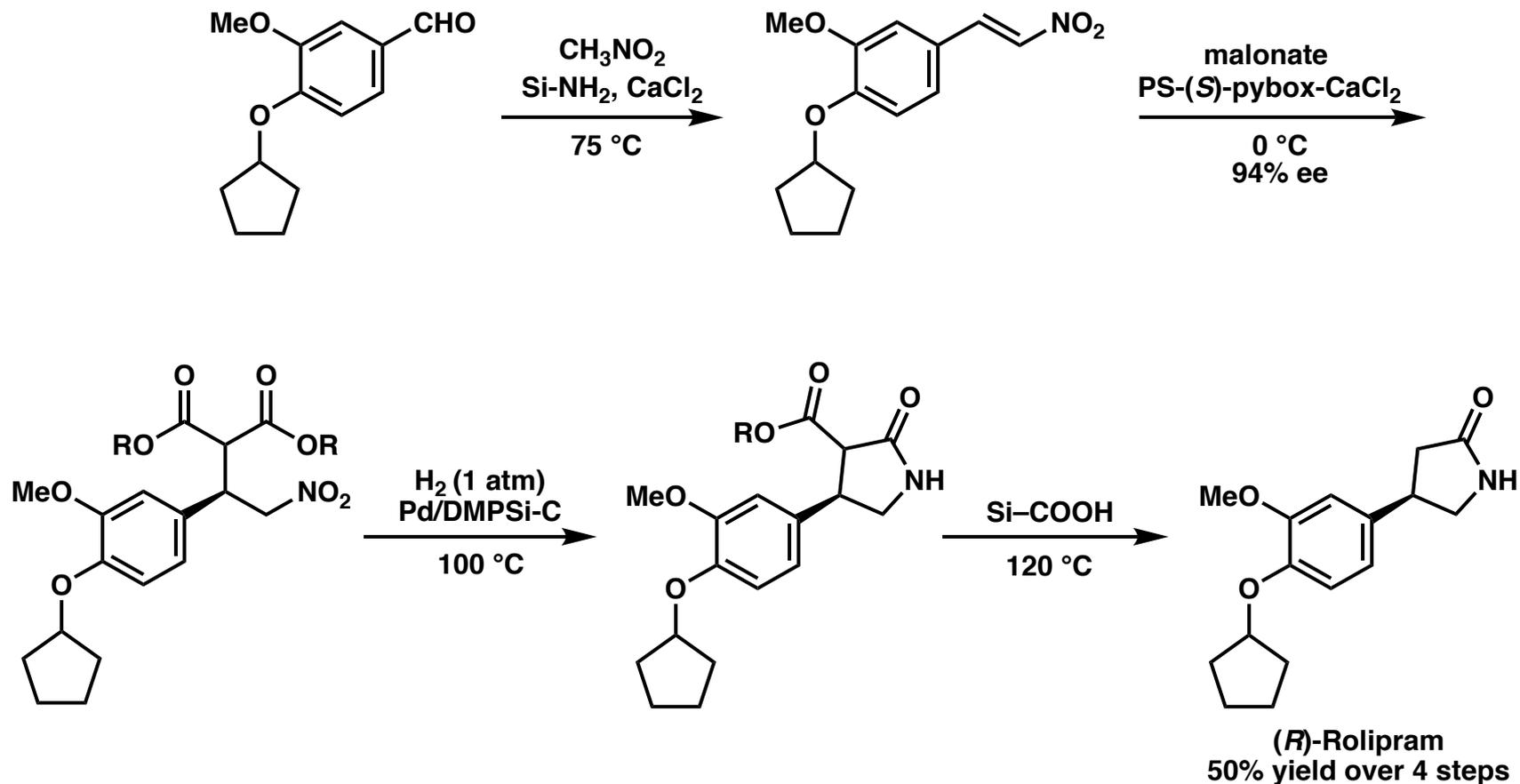


# Continuous Flow Synthesis of Ibuprofen



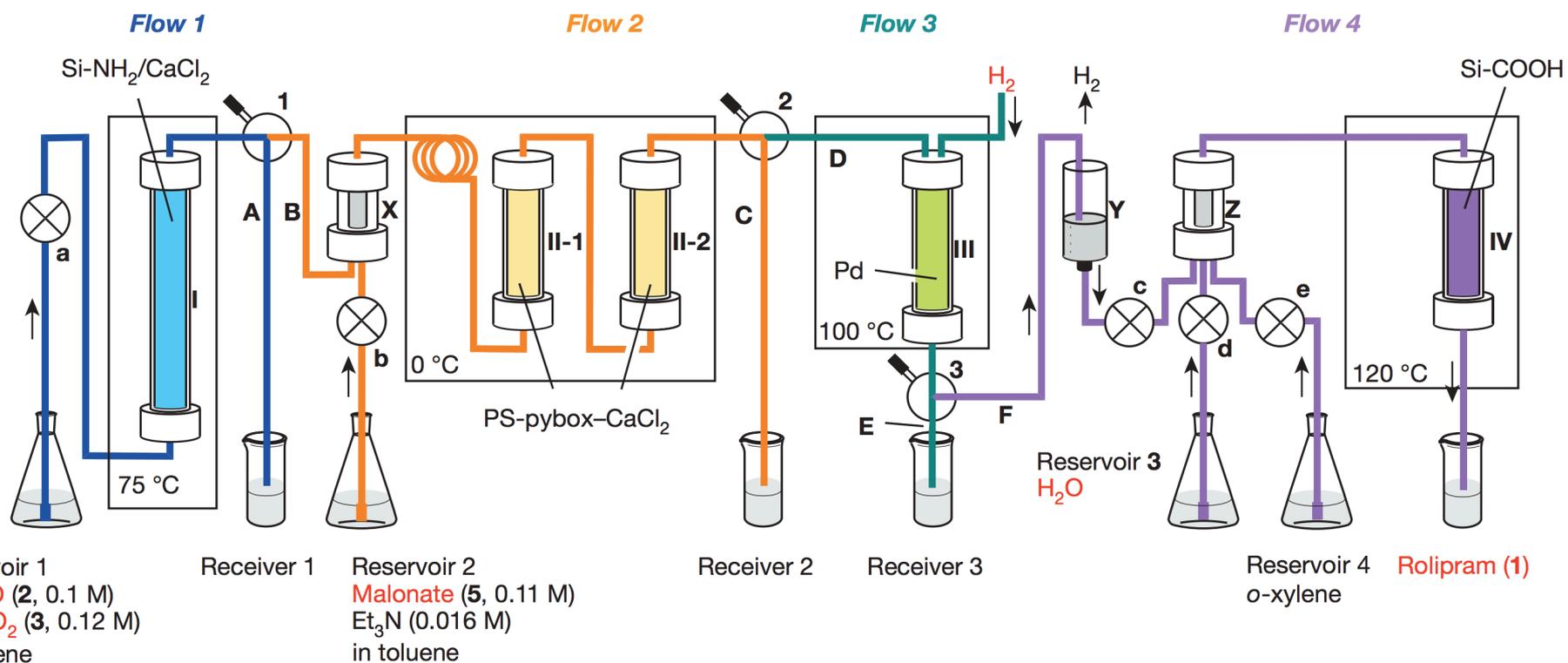


# Continuous Flow Synthesis of Rolipram

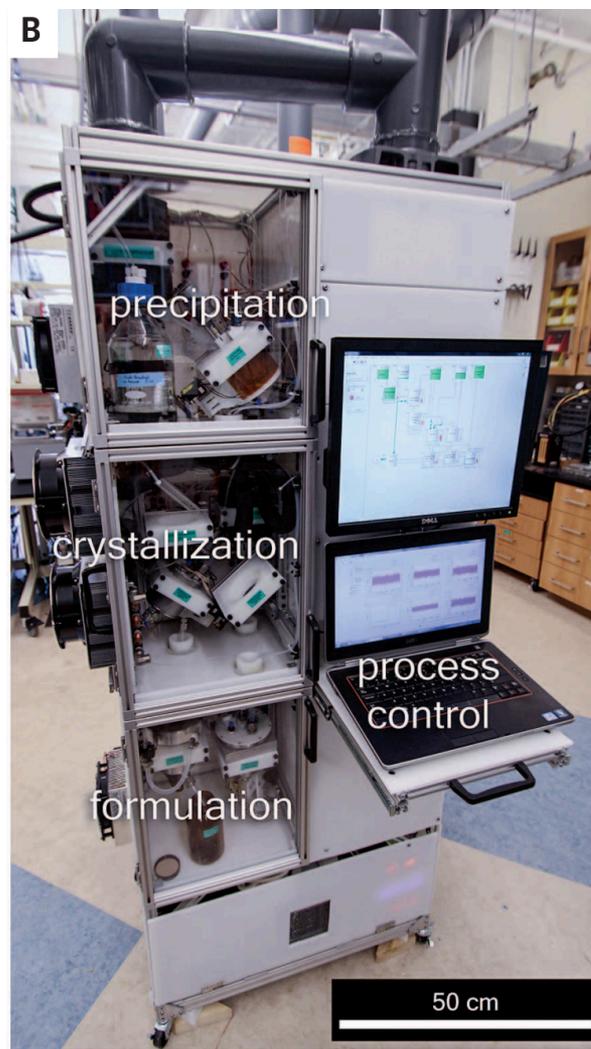
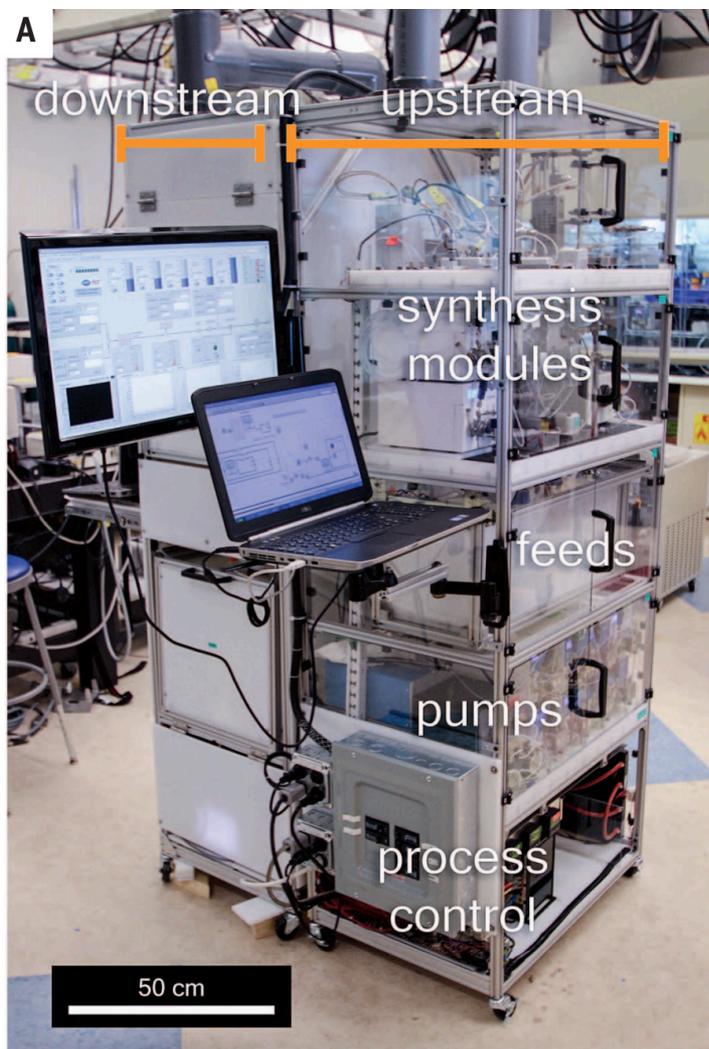


PS = polymer supported  
DMPSi-C = dimethylpolysilane

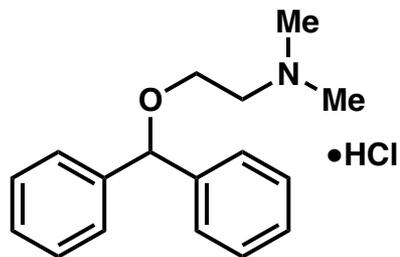
# Continuous Flow Synthesis of Rolipram



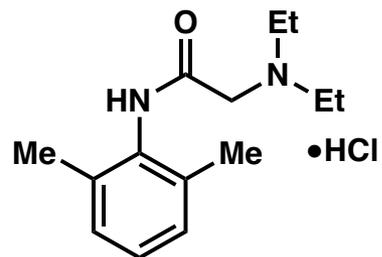
# End-to-End Continuous Manufacturing



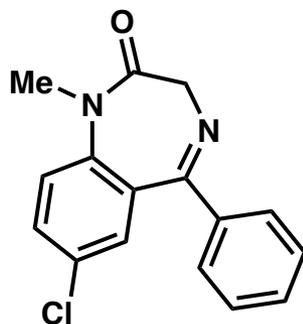
# End-to-End Continuous Manufacturing



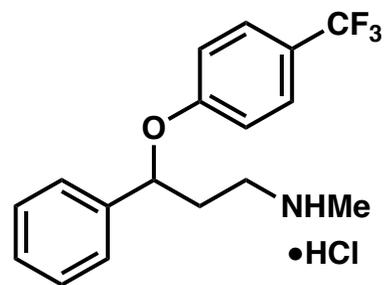
Diphenhydramine  
hydrochloride  
(Benadryl)



Lidocaine hydrochloride

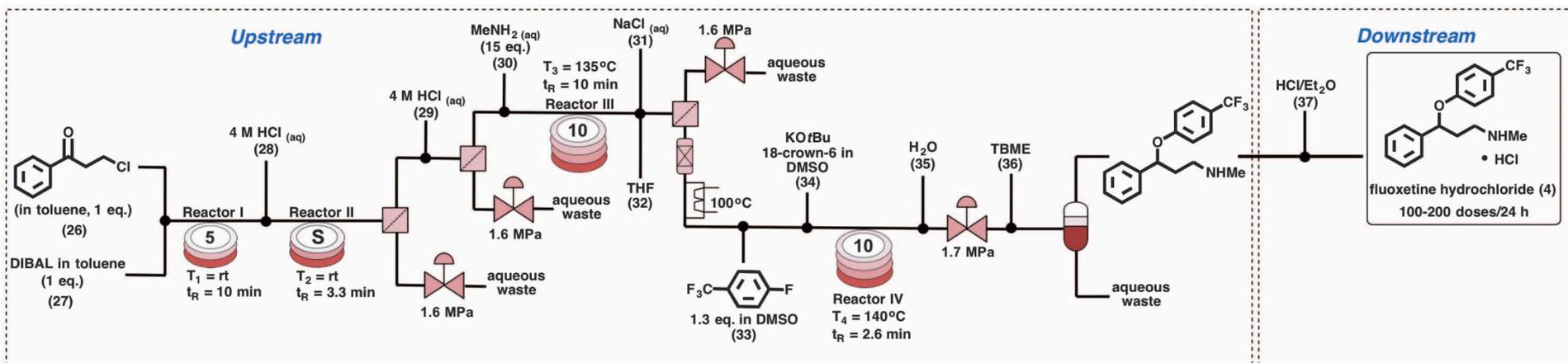


Diazepam  
(Valium)

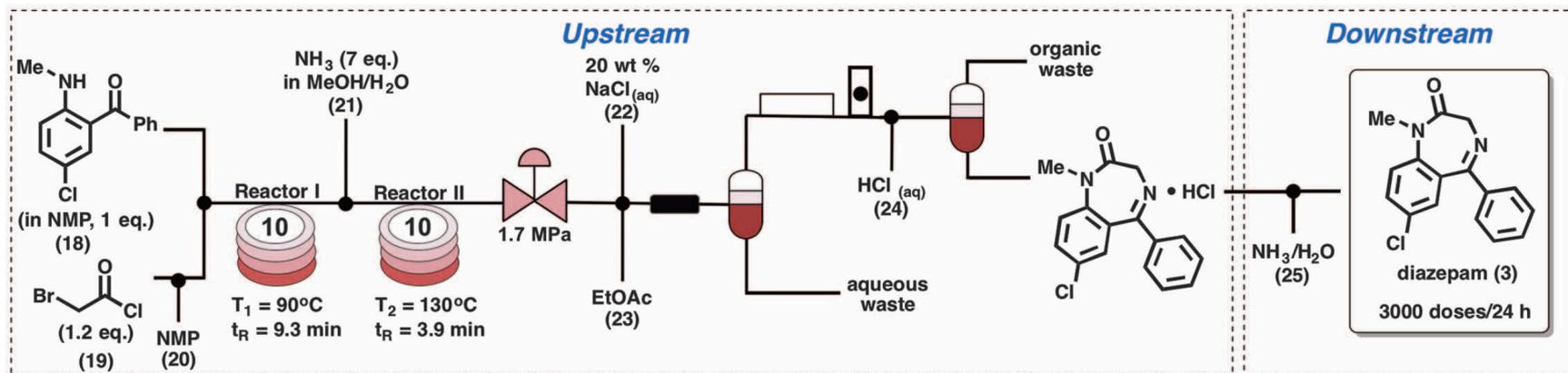
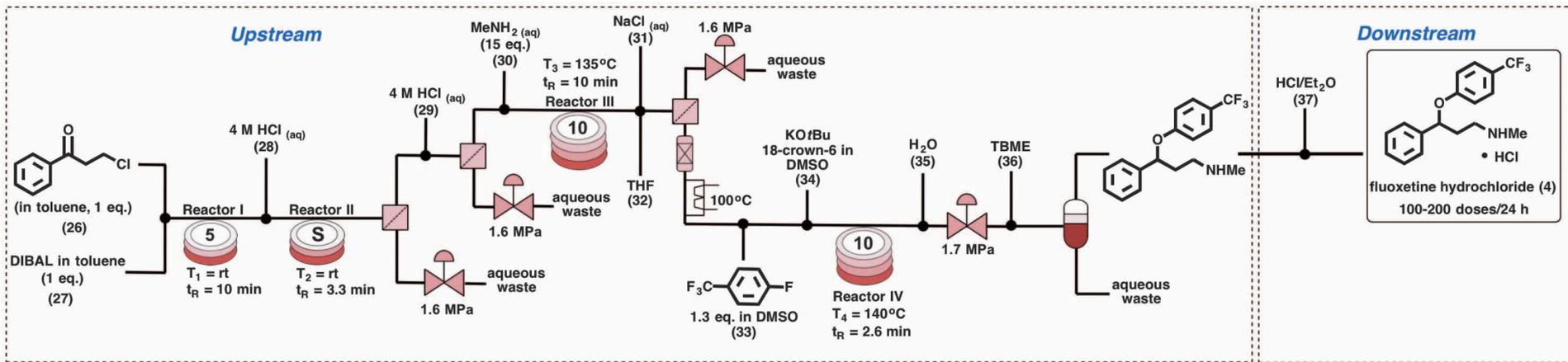


Fluoxetine hydrochloride  
(Prozac)

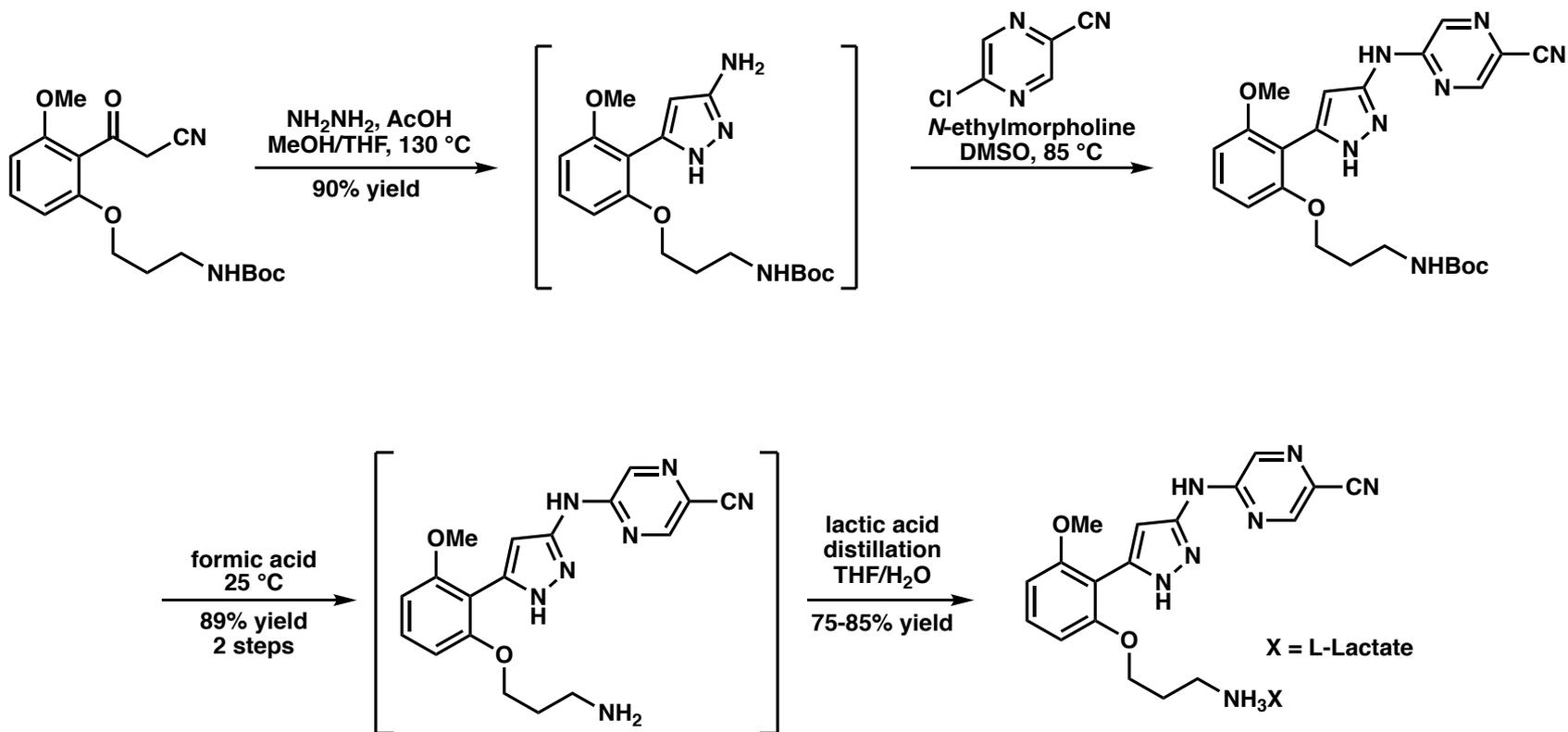
# End-to-End Continuous Manufacturing



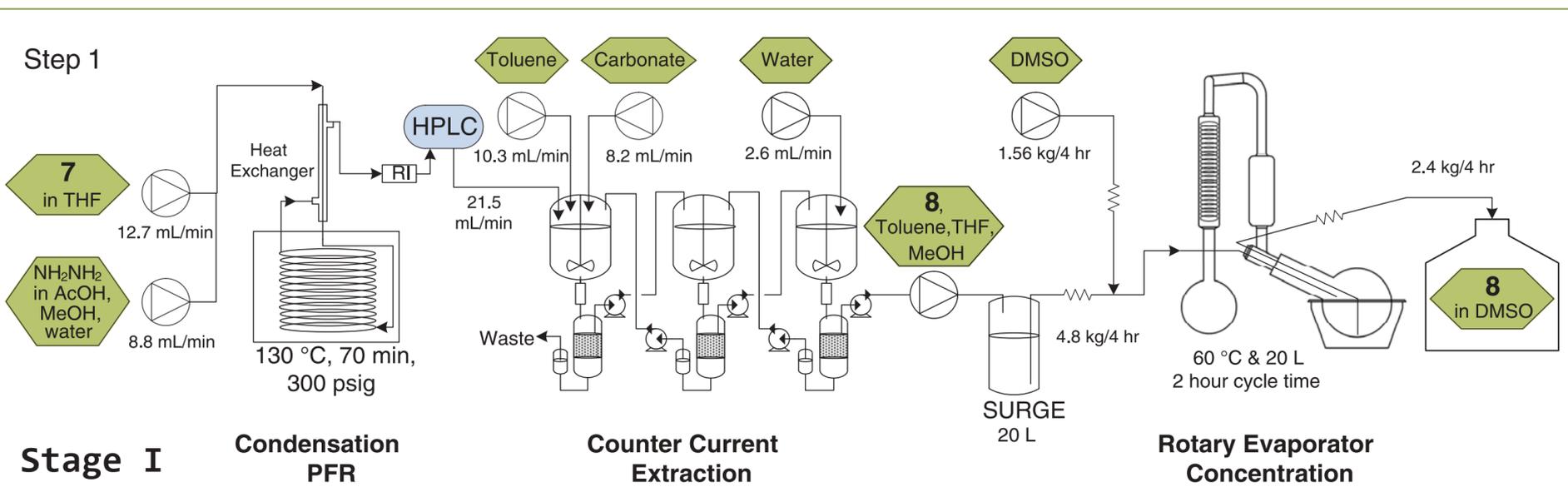
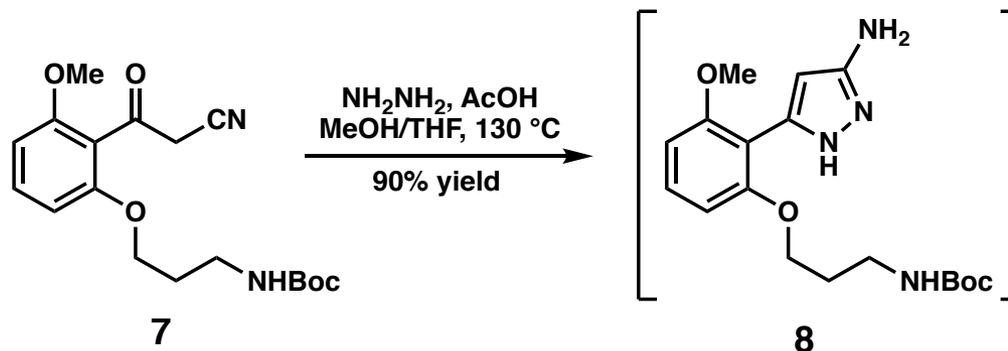
# End-to-End Continuous Manufacturing



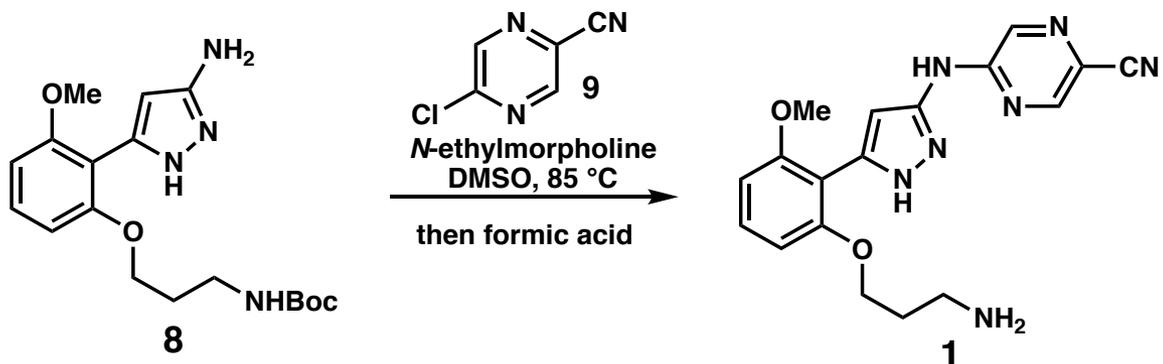
# Kilogram-scale Continuous Flow Synthesis



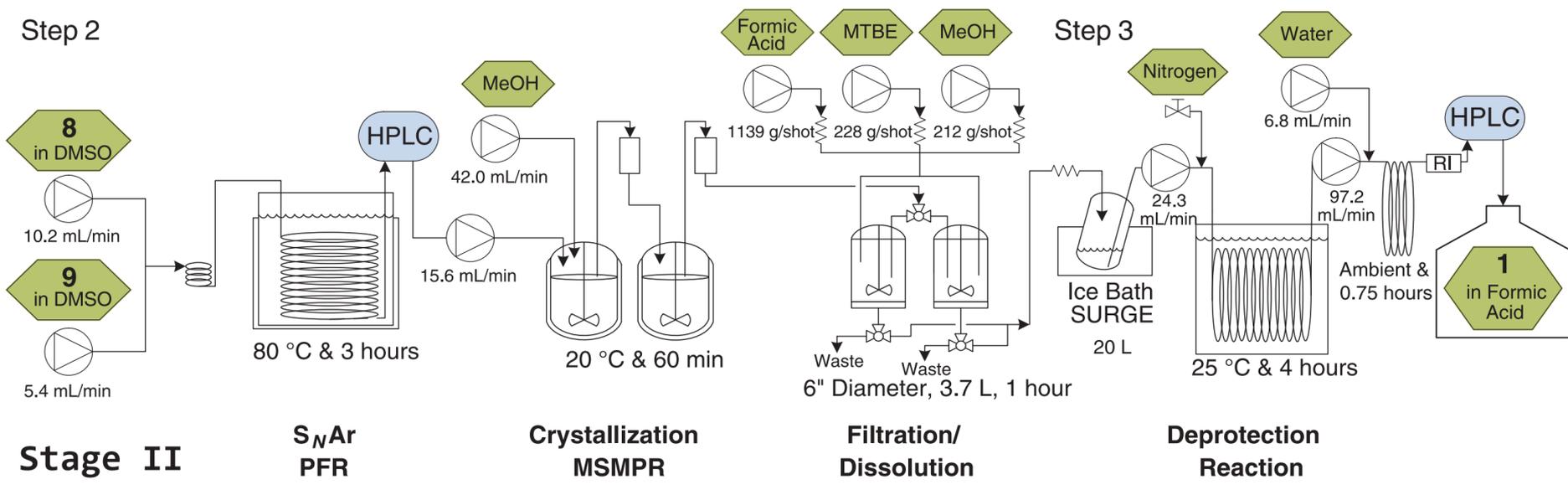
# Kilogram-scale Continuous Flow Synthesis



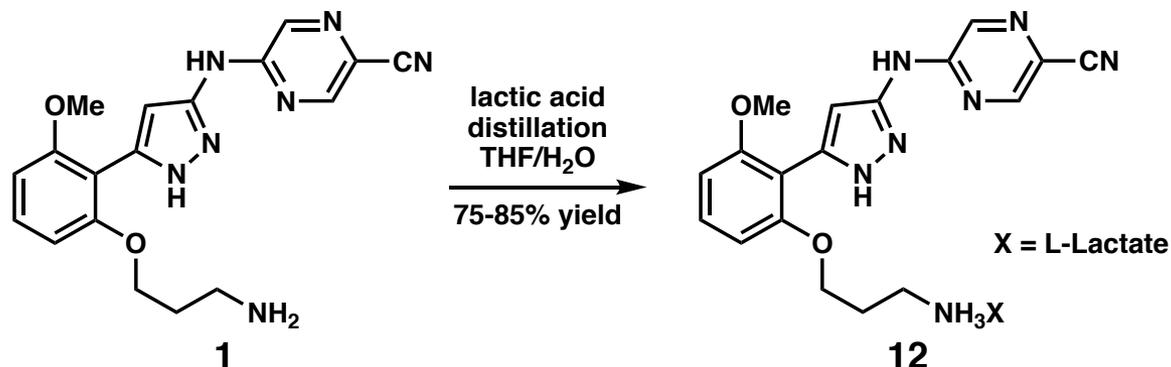
# Kilogram-scale Continuous Flow Synthesis



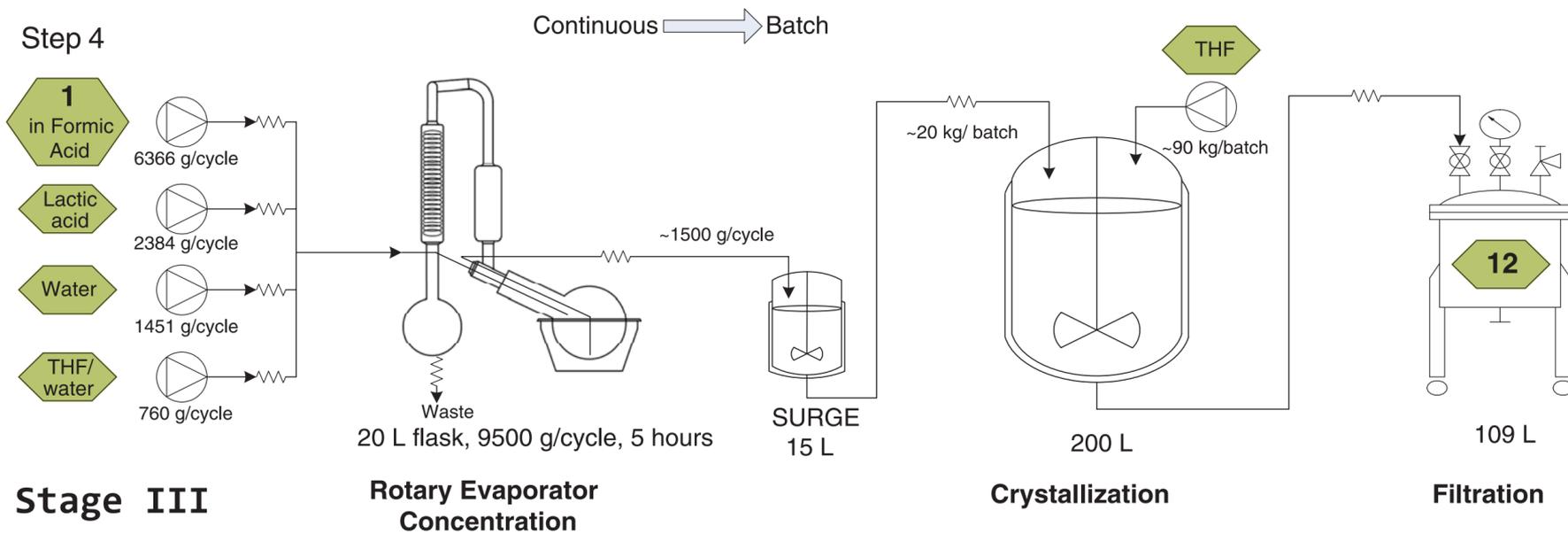
Step 2



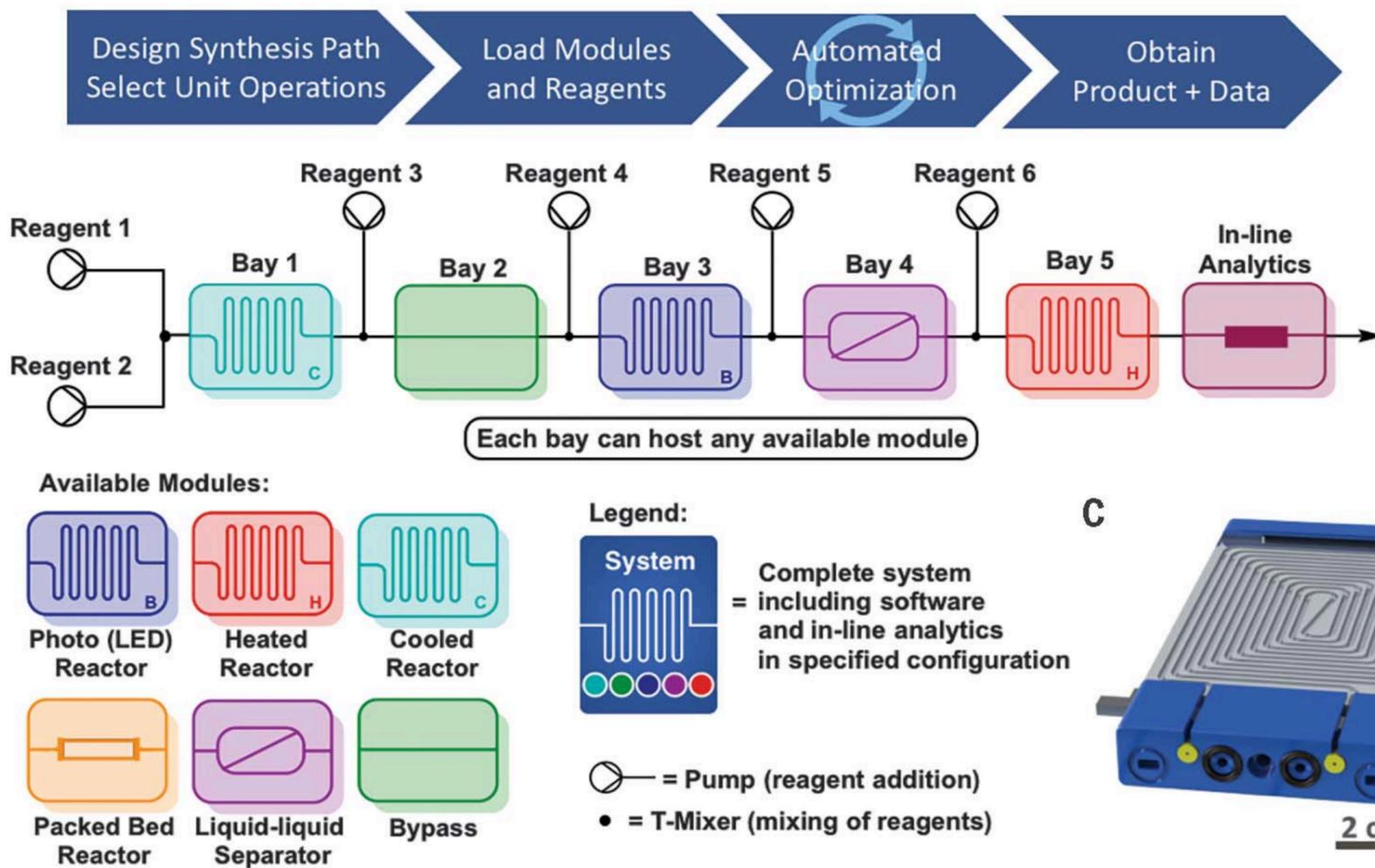
# Kilogram-scale Continuous Flow Synthesis



Step 4

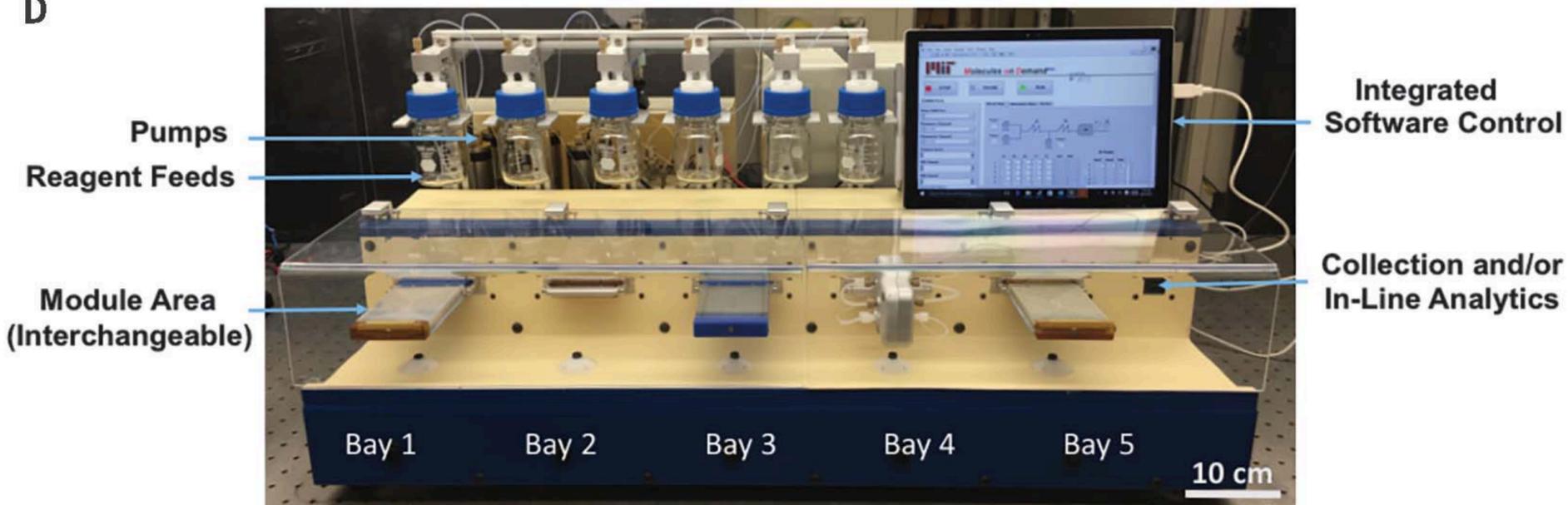


# Automated Reaction Optimization

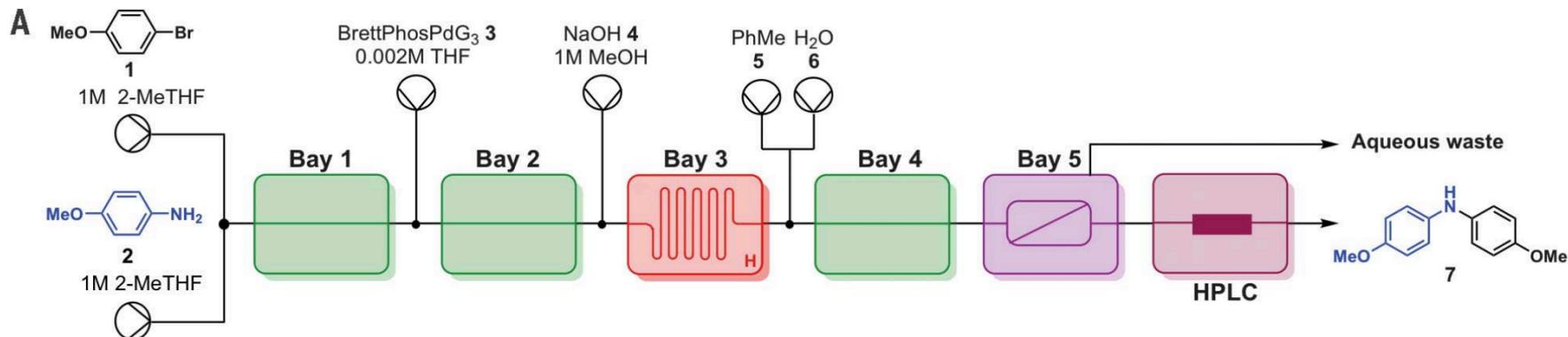


# Automated Reaction Optimization

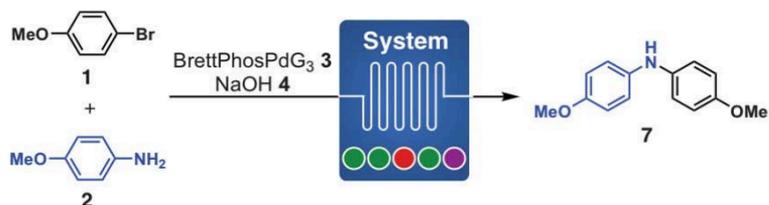
D



# Automated Reaction Optimization



## B Auto-Optimization of Buchwald-Hartwig Cross-Coupling

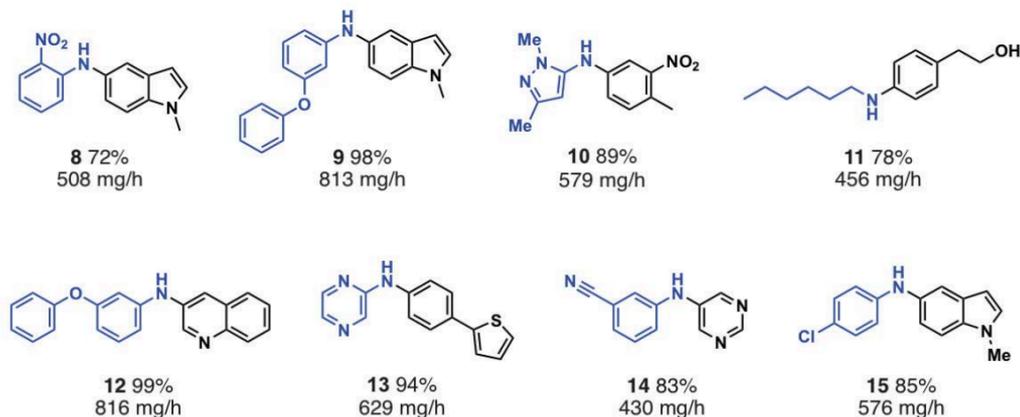


**Experiment** Number of variables optimized = 5  
Number of experiments = 32  
Total optimization time = 21 h

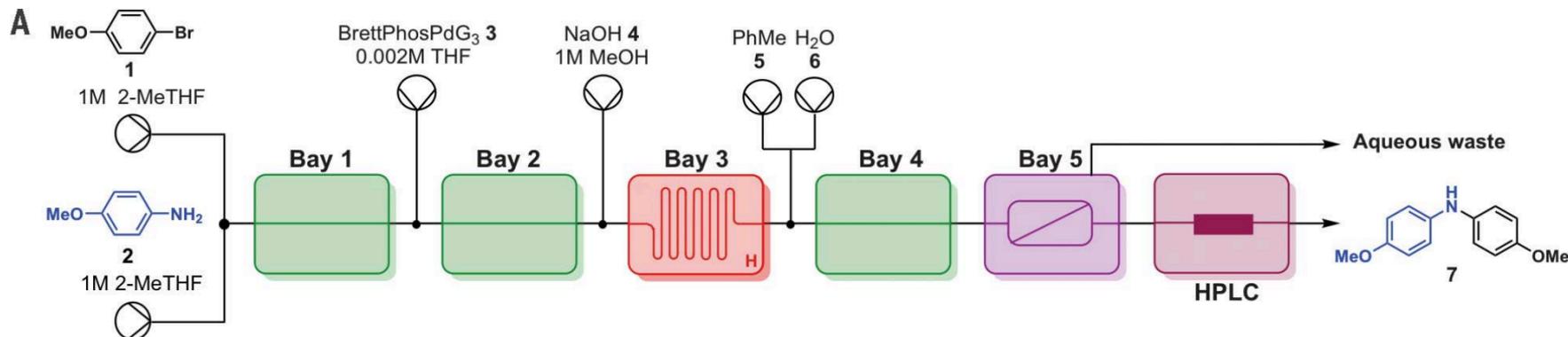
**Optimized Conditions**  
1 1.0 equiv, 2 1.2 equiv,  
3 1.4 mol%, 4 1.5 equiv  
T (Bay 3) 100 °C,  $t_R$  1.80 min

**Product (7)** 72% yield, 436 mg/h

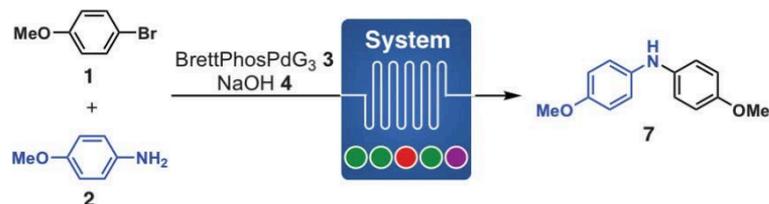
## C Substrate Scope Under Optimized Conditions



# Automated Reaction Optimization



## B Auto-Optimization of Buchwald-Hartwig Cross-Coupling

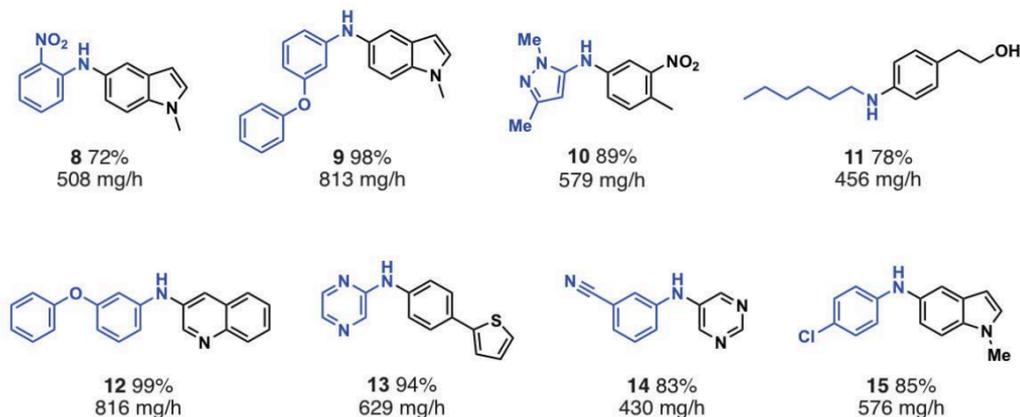


**Experiment** Number of variables optimized = 5  
Number of experiments = 32  
Total optimization time = 21 h

**Optimized Conditions**  
1 1.0 equiv, 2 1.2 equiv,  
3 1.4 mol%, 4 1.5 equiv  
T (Bay 3) 100 °C,  $t_R$  1.80 min

**Product (7)** 72% yield, 436 mg/h

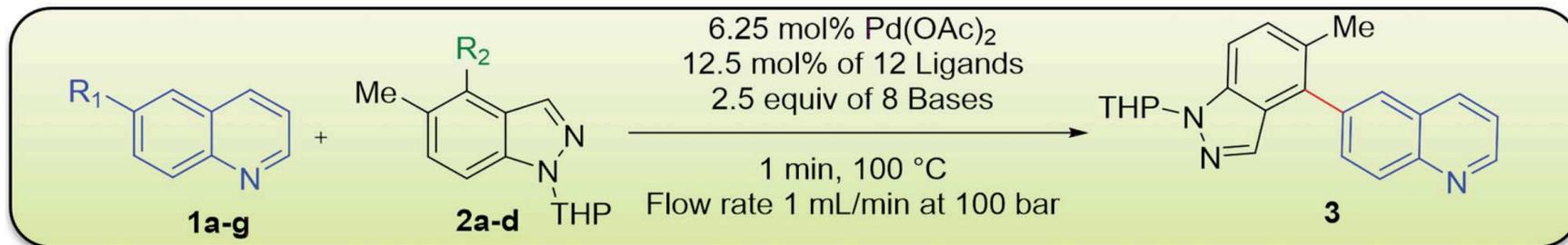
## C Substrate Scope Under Optimized Conditions



also applied to:

HWE olefination, reductive amination, Suzuki-Miyaura coupling, S<sub>N</sub>Ar, photoredox cyanation, ketene-alkene [2+2]

# Automated Reaction Optimization



## 1a-g

- 1a**  $R_1 = \text{Cl}$   
**1b**  $R_1 = \text{Br}$   
**1c**  $R_1 = \text{OTf}$   
**1d**  $R_1 = \text{I}$   
**1e**  $R_1 = \text{B(OH)}_2$   
**1f**  $R_1 = \text{Bpin}$   
**1g**  $R_1 = \text{BF}_3\text{K}$

## 2a-d

- 2a**  $R_2 = \text{B(OH)}_2$   
**2b**  $R_2 = \text{Bpin}$   
**2c**  $R_2 = \text{BF}_3\text{K}$   
**2d**  $R_2 = \text{Br}$

## Ligands:

- |   |                                |
|---|--------------------------------|
| <b>L<sub>1</sub></b> $\text{P}(t\text{Bu})_3$   | <b>L<sub>7</sub></b> SPhos     |
| <b>L<sub>2</sub></b> $\text{PPh}_3$             | <b>L<sub>8</sub></b> dtbpf     |
| <b>L<sub>3</sub></b> AmPhos                     | <b>L<sub>9</sub></b> XPhos     |
| <b>L<sub>4</sub></b> $\text{P}(\text{Cy})_3$    | <b>L<sub>10</sub></b> dppf     |
| <b>L<sub>5</sub></b> $\text{P}(o\text{-Tol})_3$ | <b>L<sub>11</sub></b> Xantphos |
| <b>L<sub>6</sub></b> CataCXium A                | <b>L<sub>12</sub></b> None     |

## Bases:

- B<sub>1</sub>** None  
**B<sub>2</sub>**  $\text{Et}_3\text{N}$   
**B<sub>3</sub>**  $\text{LiO}t\text{Bu}$   
**B<sub>4</sub>** CsF  
**B<sub>5</sub>**  $\text{K}_3\text{PO}_4$   
**B<sub>6</sub>** KOH  
**B<sub>7</sub>**  $\text{NaHCO}_3$   
**B<sub>8</sub>** NaOH

## Solvents:

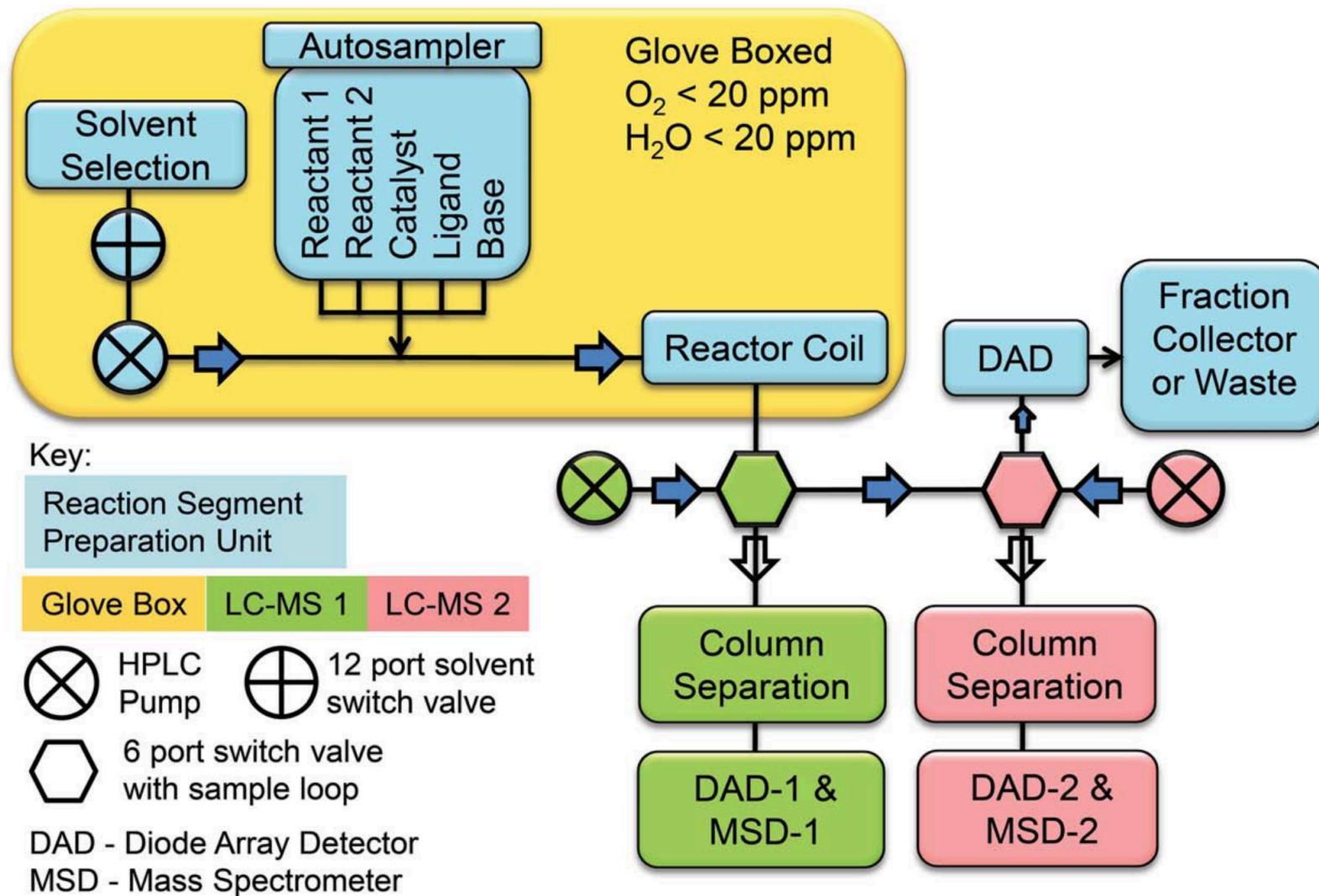
- S<sub>1</sub>** MeOH/ $\text{H}_2\text{O}$  9:1  
**S<sub>2</sub>** THF/ $\text{H}_2\text{O}$  9:1  
**S<sub>3</sub>** MeCN/ $\text{H}_2\text{O}$  9:1  
**S<sub>4</sub>** DMF/ $\text{H}_2\text{O}$  9:1

–segmented flow

–run through ~1500 reaction combinations over 24 hours

–optimization scale is 0.05 mg each reaction

# Automated Reaction Optimization



# Automated Reaction Optimization

